

# A global approach of the liquid Gibbs energy - Calphad modeling

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# Outline

- Calphad thermodynamics: basic principles
- Thermodynamic models for the liquid phase
  - Structural models
    - (Sub-) regular solutions – the Bragg-Williams model
    - Introducing short range order
      - Associate model (Predel / Sommer)
      - Modified quasi-chemical model (Chartrand / Pelton)
      - Ionic liquid model (Hillert / Sundman)
  - What about the glass transition ?
    - Two-state model (Agren)
- Conclusions

# Calphad thermodynamics : basic principles

- Thermodynamic equilibrium = Minimisation of the total Gibbs energy of the system (@ constant T,P)

$$G(T, P, x_i) = \sum_j x_j G_j(T, P, x_i)$$

$G_i$  : Gibbs energy of phase i

$T$  : temperature

$P$  : total pressure

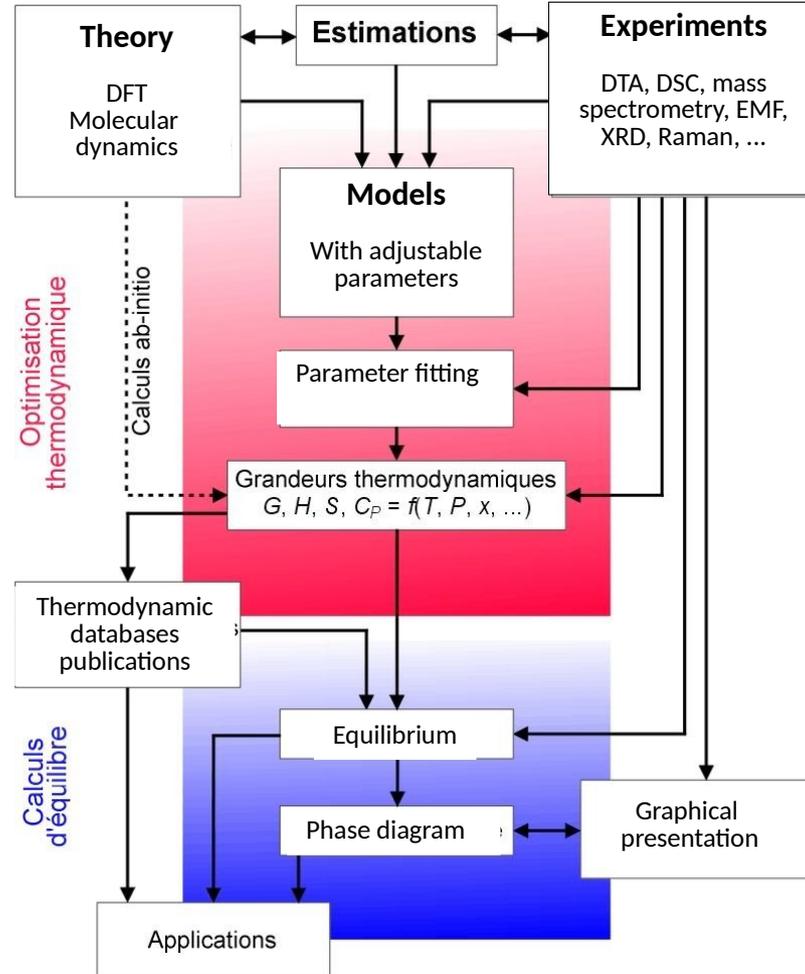
$x_i$  : composition of chemical species i

- Minimum of G with respecting mass balance + other constraints (electroneutrality ...)
- Alternative view: Phase distribution (type and amount) for which G becomes a minimum

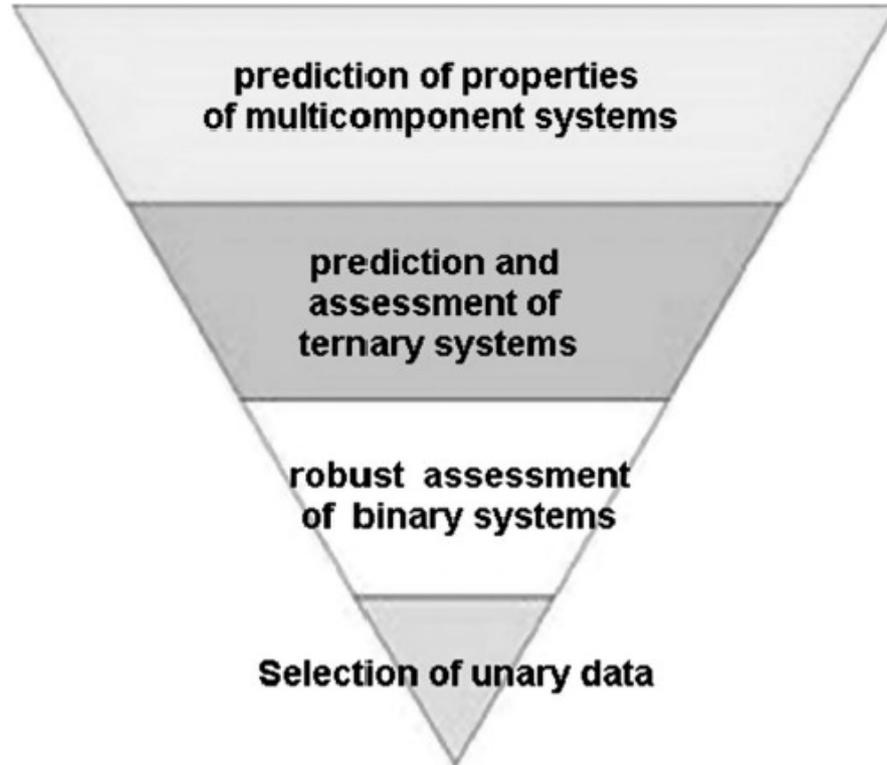
# Calphad thermodynamics : basic principles

- Gibbs energy minimization software
  - Commercial
    - Thermocalc AB
    - Factsage (GTT Technologies)
    - MTDData (Hampton Thermodynamics)
    - Pandat (CompuTherm LLC)
    - OLI [aqueous]
  - Free / Open source
    - OpenCalphad (<http://www.opencalphad.com>)
    - PyCalphad (<https://pypi.org/project/pycalphad/>)
    - GEMS (<http://gems.web.psi.ch/overview.html>) for aqueous systems
    - Phreeqc ([https://wwwbrr.cr.usgs.gov/projects/GWC\\_coupled/phreeqc/](https://wwwbrr.cr.usgs.gov/projects/GWC_coupled/phreeqc/)) for aqueous systems

# Calphad thermodynamics : basic principles



# Calphad thermodynamics : database development



## Unary data

- Elements (Al, Hg, O<sub>2</sub>(g) ...)
- Simple Oxides (CaO, Al<sub>2</sub>O<sub>3</sub>, SiO<sub>2</sub>,...)
- Halides (NaCl, CaCl<sub>2</sub>)
- Sulfates ; Phosphate ; Hydroxides ; ....

# Calphad thermodynamics : database development

$$G = \Delta H - T * S$$

$$\Delta H(T) = \Delta H(0K) + \int_{0K}^T C_p dT$$

$$S(T) = S(0K) + \int_{0K}^T \frac{C_p}{T} dT$$

$$C_p = a + b * T + c * T^2 + d * \frac{1}{T^2}$$

## Stoichiometric compounds

- Elements: Mg, Si, O<sub>2</sub>(g) ...
- Compounds: CaSi<sub>2</sub>, MgO, NaCl...
- End members of solutions (!)

# Calphad thermodynamics : database development

## Complex gas phase

- Ideal gas  $pV=nRT$

$$G^{gas} = \sum_i^n x_i \left( G_i^0 + RT \ln \left( \frac{P_i}{P^0} \right) \right)$$

$P_i$  partial pressure of gas species  $i$

$P^0$  reference total pressure

# Calphad thermodynamics: database development

## Solution phases

- Solid solutions
  - Disordered : e.g. FCC\_A1, BCC\_A2 ...
  - Ordered phases : e.g. L1<sub>2</sub>
- Liquid solutions
  - Molecular
    - weak interaction, v.d. Waals: H<sub>2</sub>O
  - Metallic
    - atomic distribution in an electron cloud: Au-Ag
  - Covalent
    - strong structural aspect: SiO<sub>2</sub>
  - Ionic
    - Coulombian forces, electronic charges & ion radius: molten salts
  - Other
    - Polymers, liquid crystals

# Thermodynamic modeling of the liquid phase

Gibbs energy of any solution is additive:  $G^{sol} = G^{ref} + G^{id} + G^{exc}$

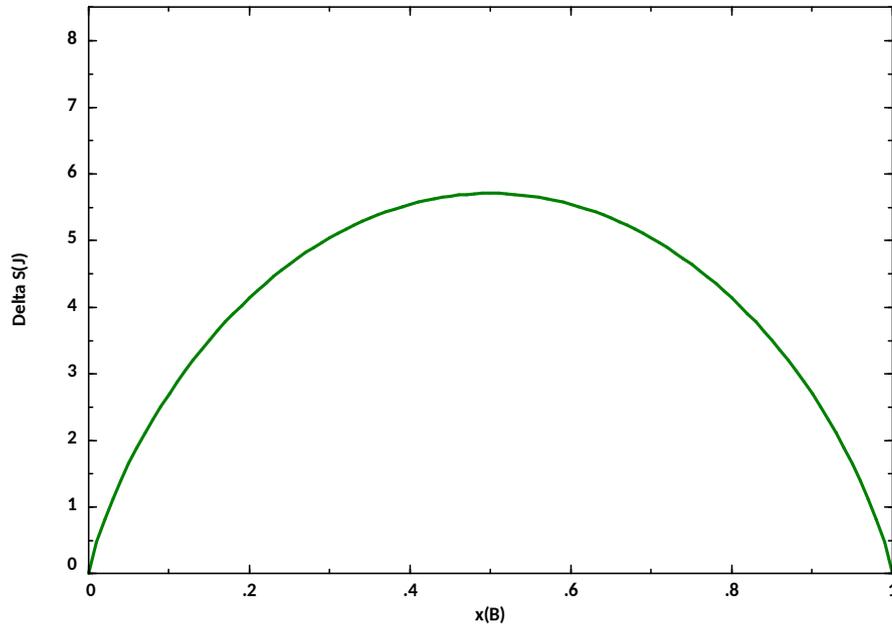
$G^{ref} = \sum_i x_i G_i^0(T, P, x_i)$  Reference Gibbs energy “mechanical mixture”

$G^{id} = T * S^{id} = RT \sum_i x_i \ln(x_i)$  Ideal mixing

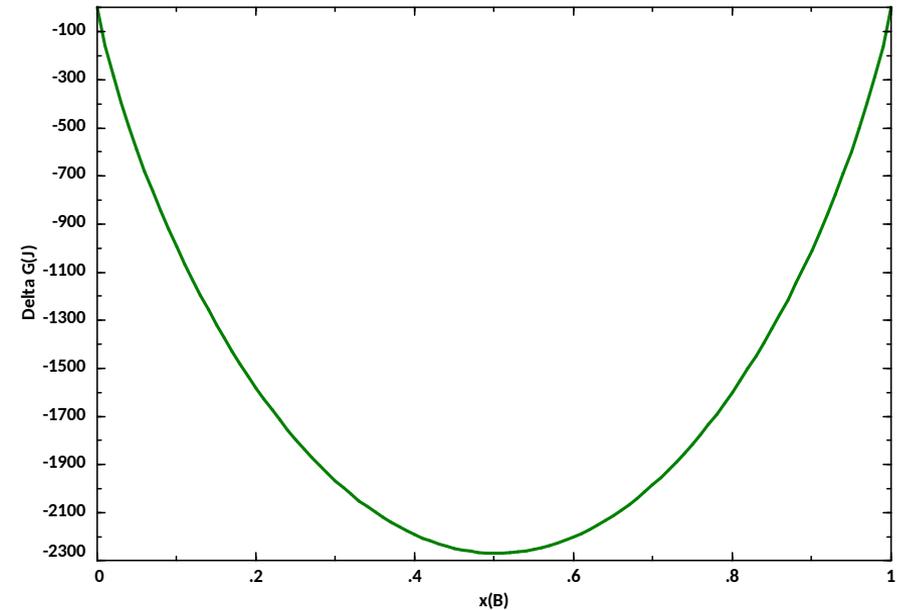
$G^{exc}$  Excess Gibbs energy due to mixing

# Thermodynamic modeling of the liquid phase

$$G^{id} = T * S^{id} = RT \cdot \sum_i x_i \ln(x_i)$$



Ideal entropy



resulting Gibbs energy @420K

# Model : (Sub-)regular solution

- Enthalpy difference between A+B and solution (AB)  $\neq 0$   
→ mixing generates or consumes heat
- The molar enthalpy of the solution can be evaluation from the pair interaction

$$[A-A]_{\text{pair}} + [B-B]_{\text{pair}} = 2 [A-B]_{\text{pair}}$$

with the total energy for two pairs:  $\Delta E_{AB} = 2 E_{AB} - E_{AA} - E_{BB}$

one gets for the mixing energy  $G^{\text{exc}} = x_A x_B \omega_{AB}$  → regular solution

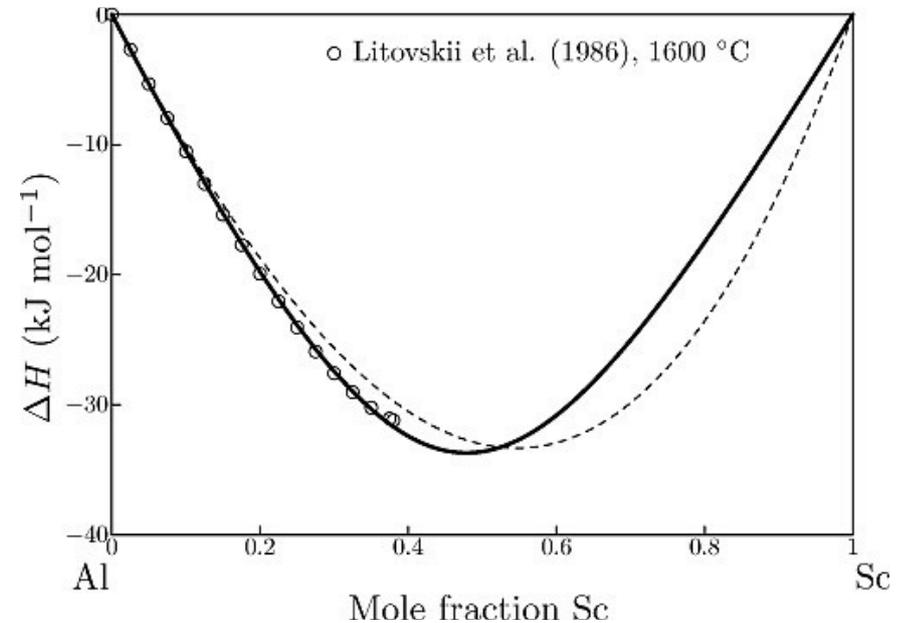
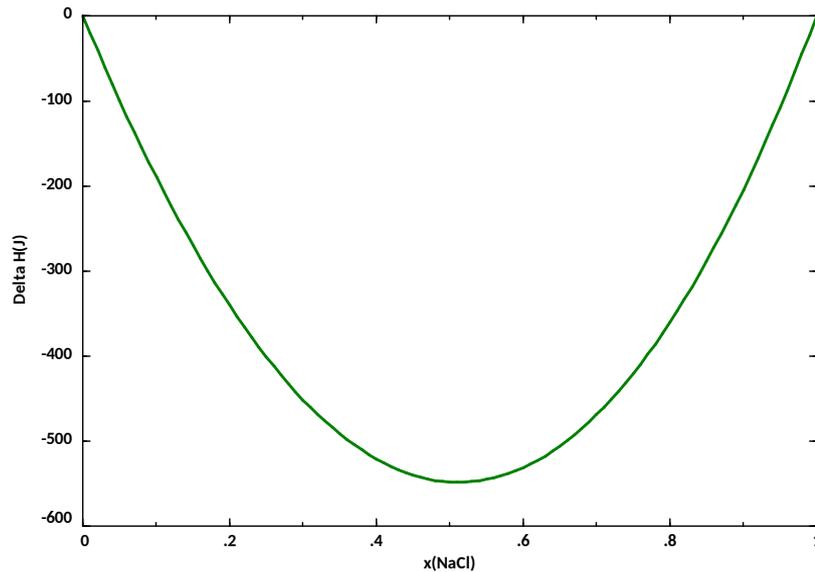
$\omega_{AB}$  can

- be a constant = configurational entropy is ideal
- depend on temperature = configurational entropy is taken into account
- depend on other parameters (pressure, ionic radius...)

# Model : (Sub-) regular solution

- Chemically similar species can be described by a regular solution model
- model can be applied for solid and liquid phases
- interaction is weak and very low tendency for short range order

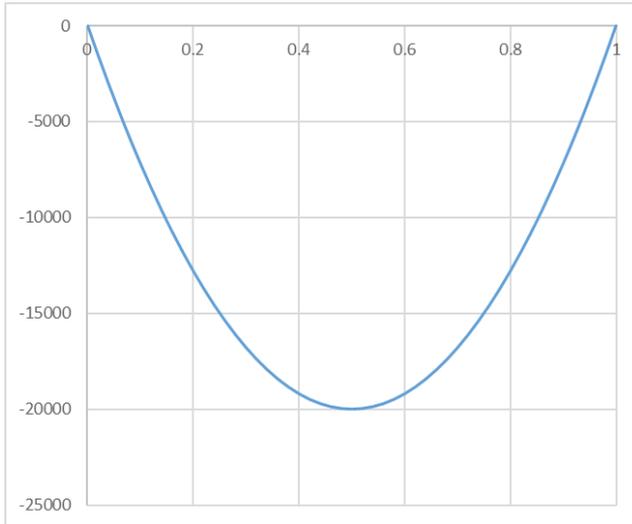
*<A> NaCl + <1-A> KCl*



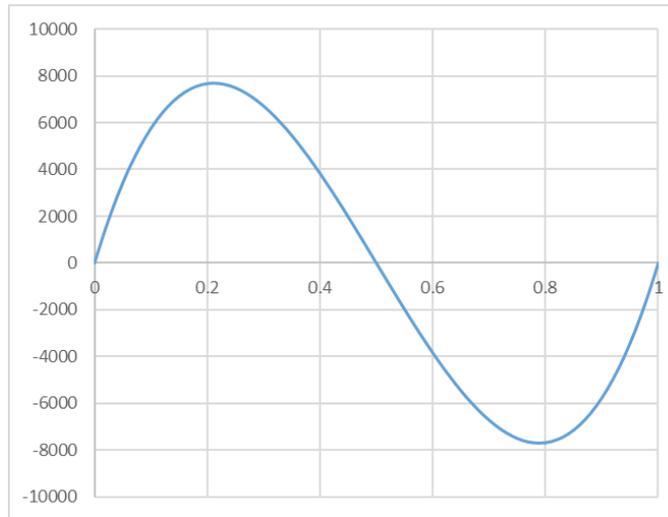
# Model : (Sub-) regular solution

Redlich Kister polynomials

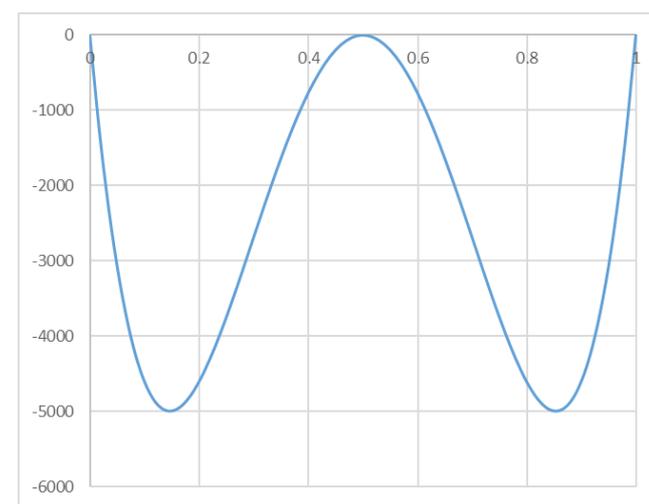
$$G^{exc} = x_A x_B \sum_0^n (x_A - x_B)^n L_{AB}^n$$



n=0



n=1

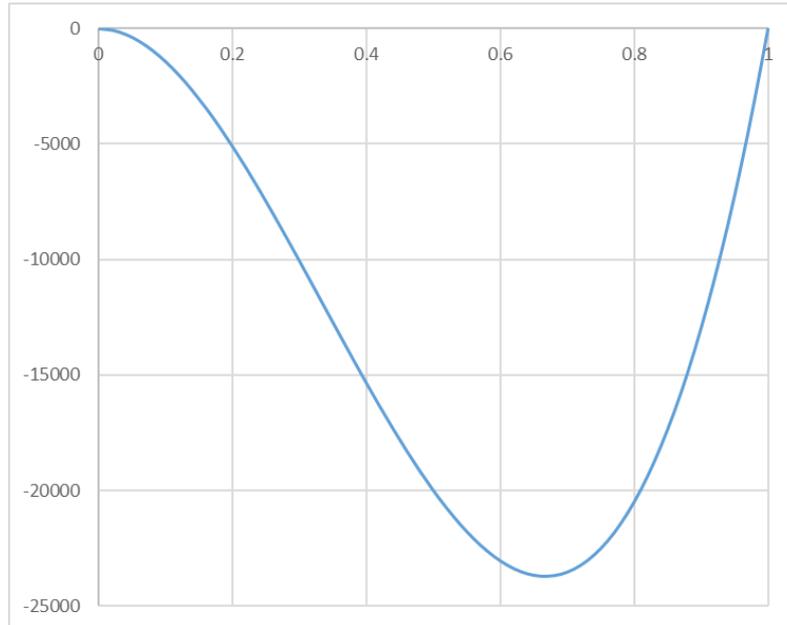


n=2

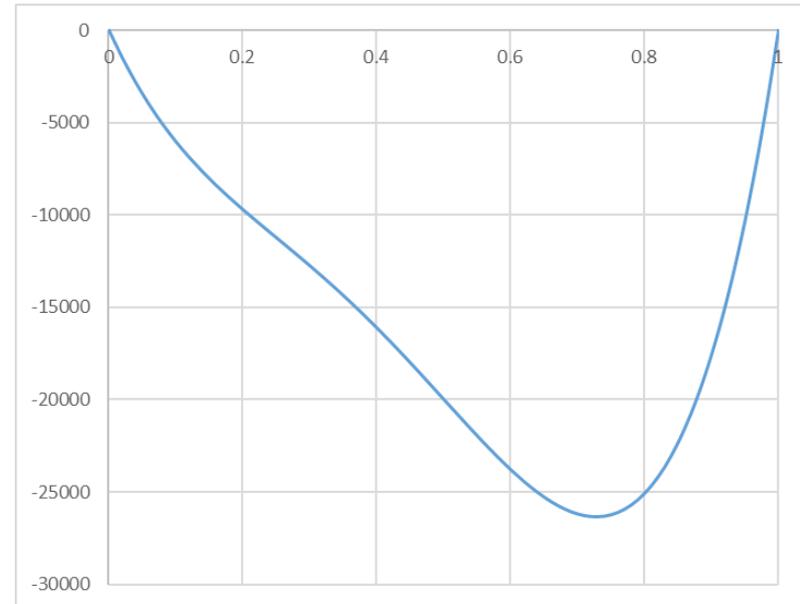
# Model : (Sub-) regular solution

Redlich Kister polynomials

$$G^{exc} = x_A x_B \sum_0^n (x_A - x_B)^n L_{AB}^n$$

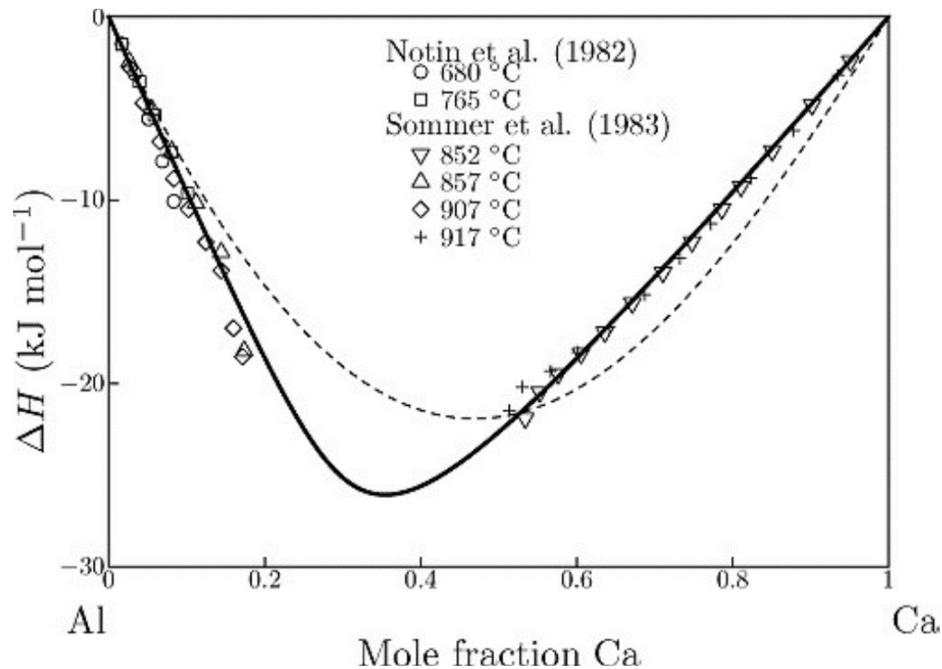


n=0,1



n=0,1,2

# Calphad modeling: (Sub-) regular solution



# Short range ordering

- (Sub-) regular model is not suited for systems with strong tendency for short range order
  - Al-Y, Mg-Si ...
  - Metal-oxide (Ca-CaO), metal-fluoride ...
  - Oxide-oxide system ( $\text{Na}_2\text{O-SiO}_2$ ,  $\text{Na}_2\text{O-Al}_2\text{O}_3$ ,...)
  - Reciprocal systems:  $\text{NaF-CaF}_2\text{-NaCl-CaCl}_3$
- Models to describe short range order
  - Associate model (Predel / Sommer)
  - Quasi-chemical model (Fowler / Guggenheim / Pelton / Blander / Chartrand)
  - Ionic liquid model (Hillert/Sundman)

# Short range ordering : associate model

- Model developed by Predel & Sommer (Univ. Stuttgart, Germany)
- Basic assumption
  - Two species are “bound” together (= form an associate) so that they can be considered as an individual particle/complex
- The Gibbs energy for the solution phase becomes (e.g. associate AB)

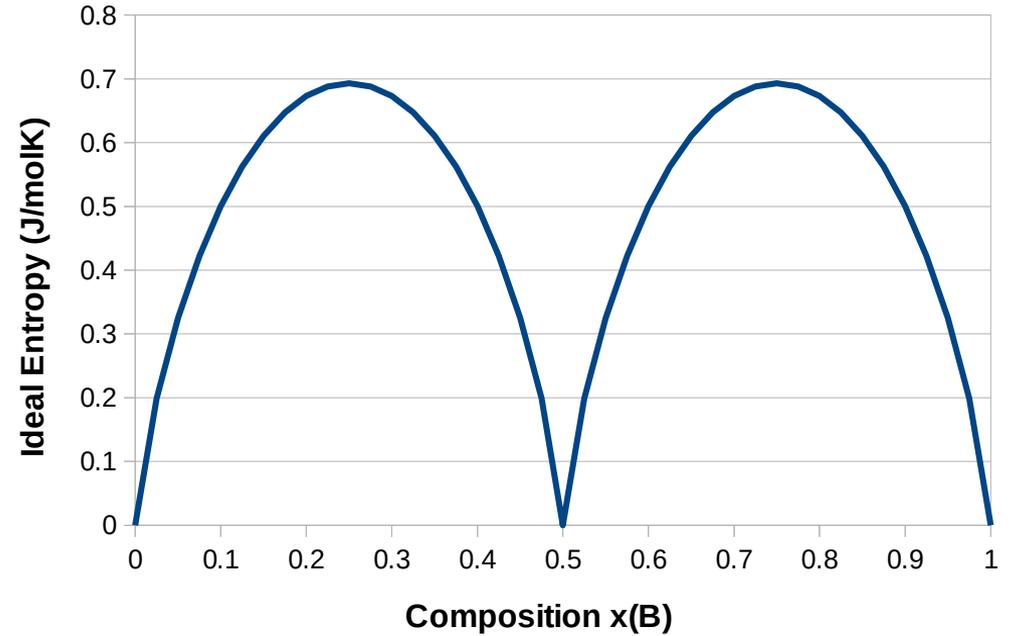
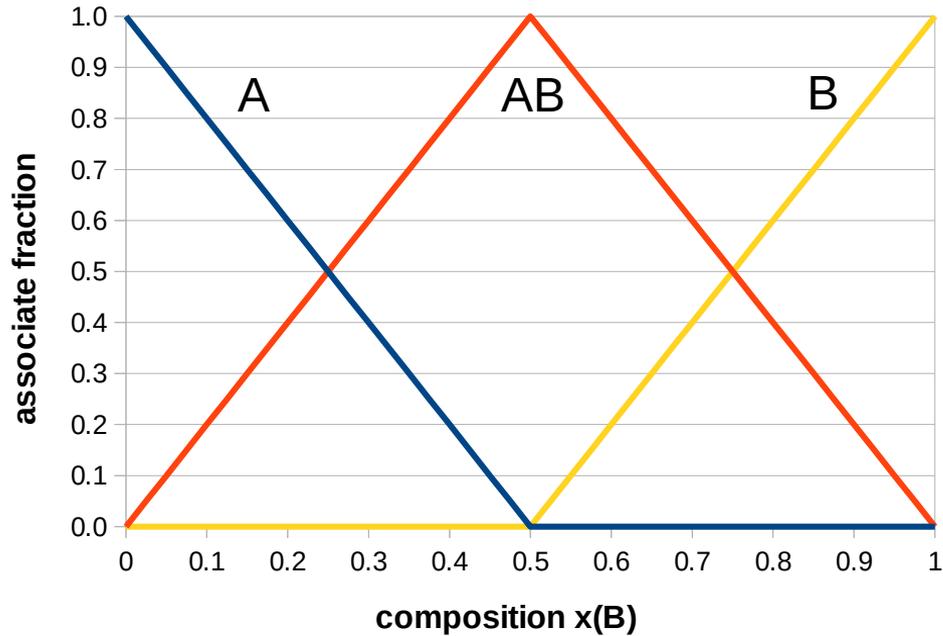
$$G^{ref} = \sum_i x_i G_i^0(T, P, x_i)$$

$$i = A, B, AB$$

$$G^{id} = T * S^{id} = RT \sum_i x_i \ln(x_i)$$

$$G^{exc} = x_A x_B \sum_0^n (x_A - x_B)^n L_{A-B}^n + x_A x_{AB} \sum_0^n (x_A - x_{AB})^n L_{A-AB}^n + x_{AB} x_B \sum_0^n (x_{AB} - x_B)^n L_{AB-B}^n$$

# Short range ordering : associate model



# How to choose the associates ?

- The choice of the associates is arbitrary and have not always a physical meaning !
- Ideally, start from experimental information

- Raman
- NMR
- XANES
- ...

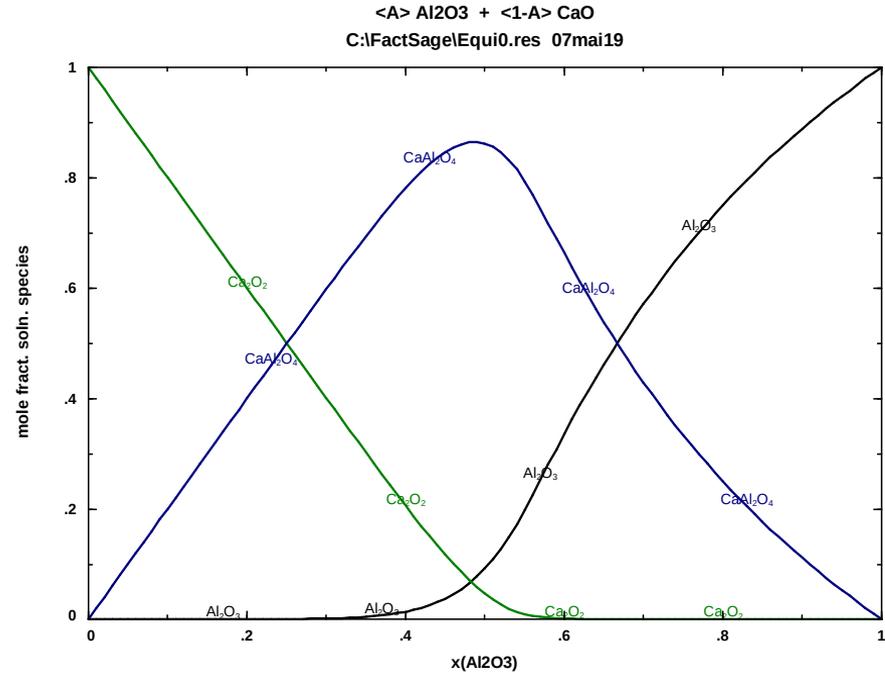
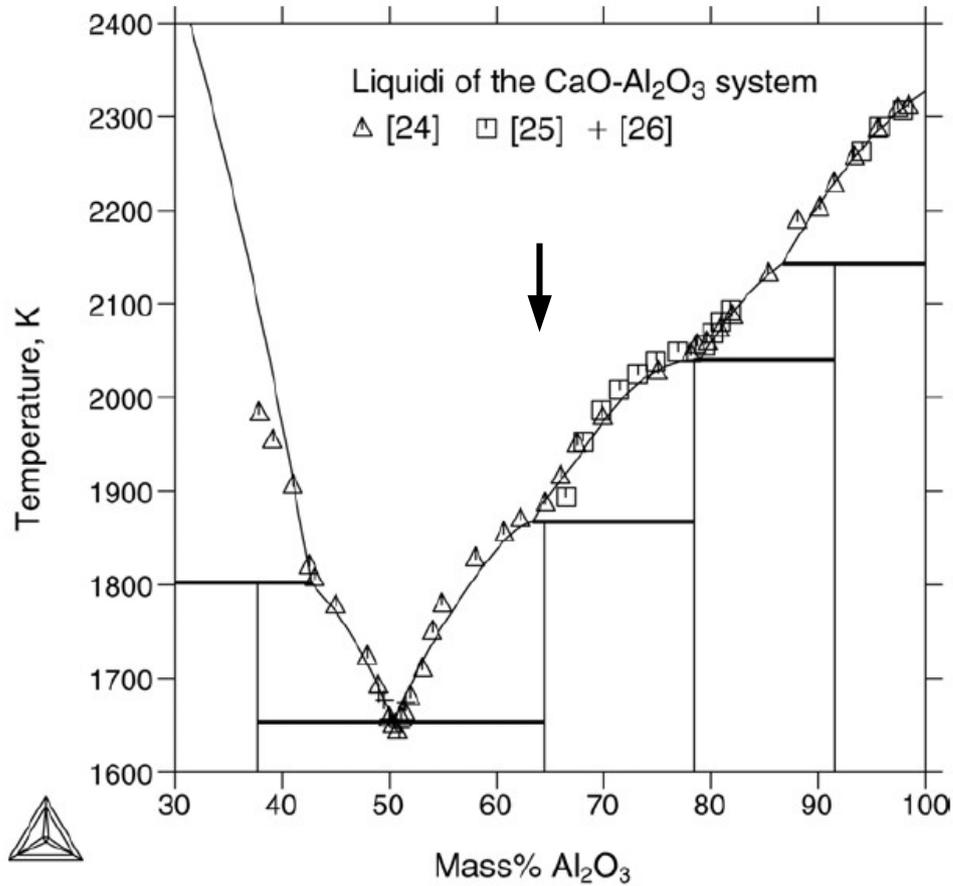


Q<sup>n</sup>-species

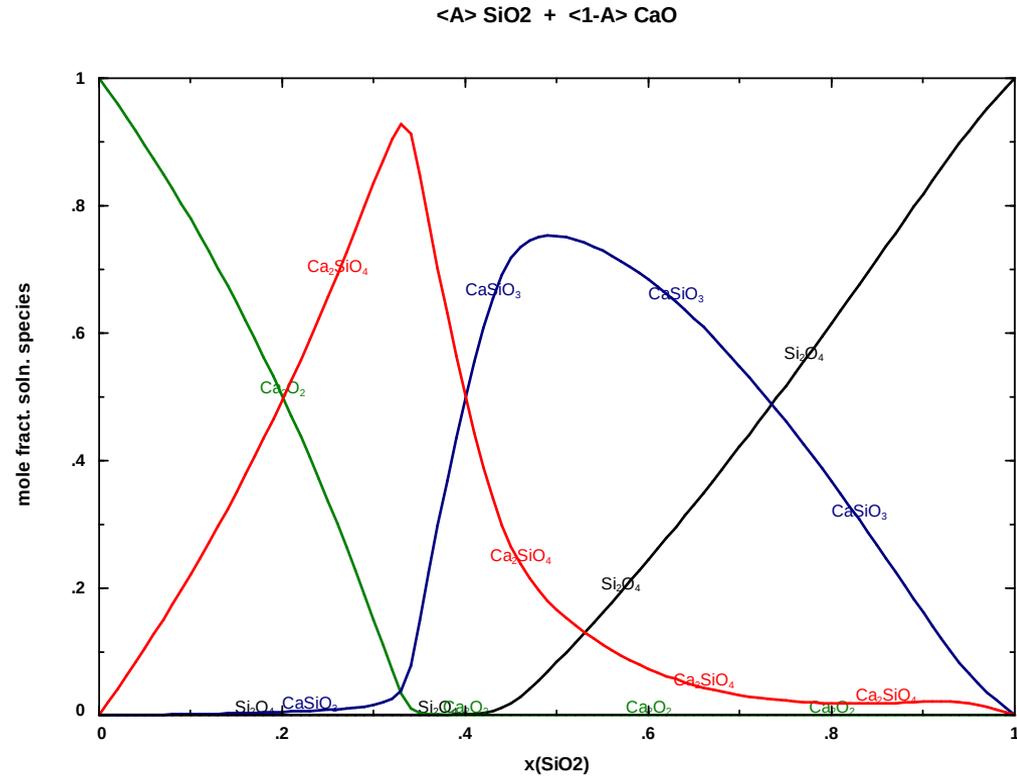
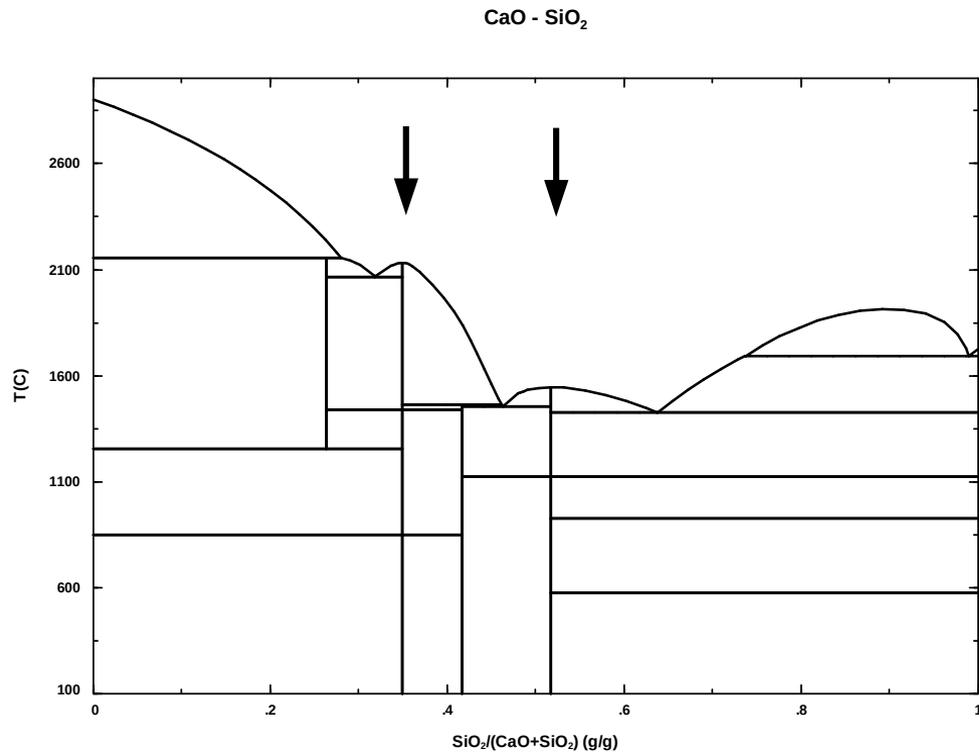
- Examples

- GTOx:  $\text{Ca}_2\text{O}_2$ ,  $\text{Si}_2\text{O}_4$ ,  $\text{Al}_2\text{O}_3$ ,  $\text{Na}_2\text{O}$ ,  $2/3 \text{Ca}_2\text{SiO}_4$ ,  $\text{CaSiO}_3$ ,  $2/3 \text{CaAl}_2\text{O}_3$ ,  $2/5 \text{Na}_4\text{SiO}_4$  ...
- MTOx:  $\text{CaO}$ ,  $\text{AlO}_{3/2}$ ,  $\text{SiO}_2$ ,  $\text{MgO}$ ,  $\text{CaSiO}_3$ ,  $\text{SiAl}_{4/3}\text{O}_4$ ...

# Associate model : $\text{CaO-Al}_2\text{O}_3$



# Associate model : $\text{CaO-SiO}_2$



Potential associates:  $\text{CaO}$ ,  $\text{Al}_2\text{O}_3$

# Short range ordering : Quasi-chemical model

## Impact of the pair interaction on the configuration

– Introduced by Fowler & Guggenheim (1939)

- The configurational entropy and the mixing enthalpy depend on the pair interaction energy

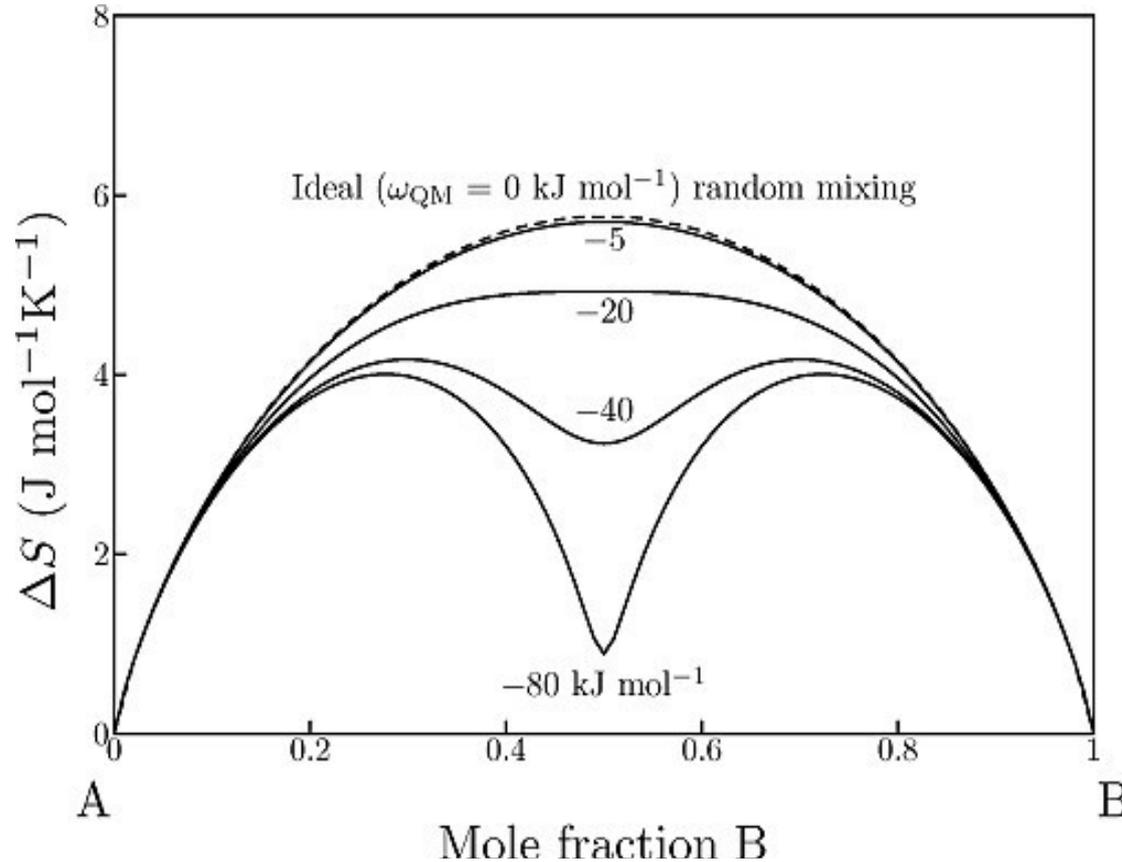
$$[A-A]_{\text{pair}} + [B-B]_{\text{pair}} = 2 [A-B]_{\text{pair}} \quad \Delta g_{AB} = \omega_{AB} - \eta_{AB} T$$

- Allows to evaluate the short range order tendency of a solution
- The configurational entropy expression is derived from the Ising model

$$S^{\text{config}} = -R(x_A \ln(x_A) + x_B \ln(x_B)) - R(x_{AA} \ln\left(\frac{x_{AA}}{x_A^2}\right) + x_{BB} \ln\left(\frac{x_{BB}}{x_B^2}\right) + x_{AB} \ln\left(\frac{x_{AB}}{x_A x_B}\right))$$

- If  $\omega_{AB} = 0$ , the configuration entropy becomes identical to the ideal entropy

# Short range ordering : Quasi-chemical model

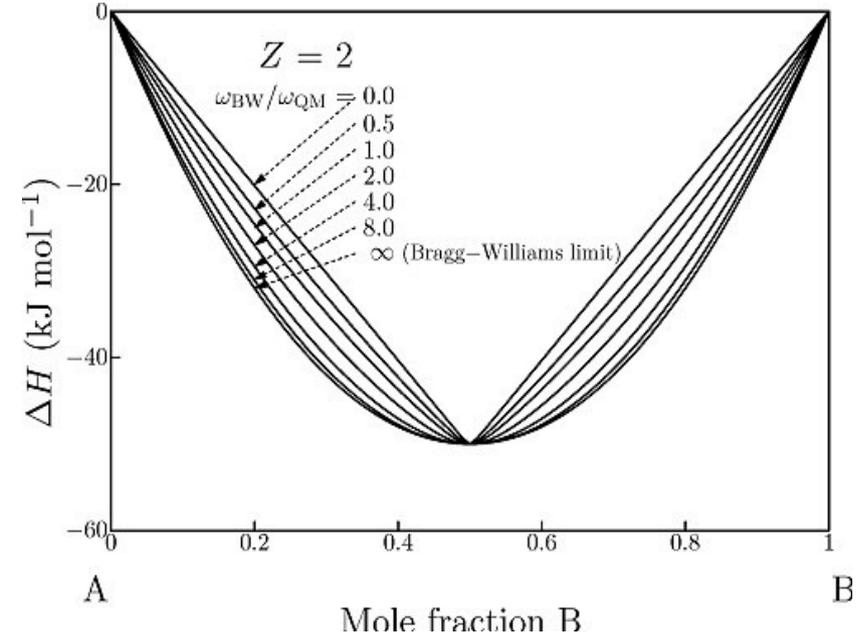
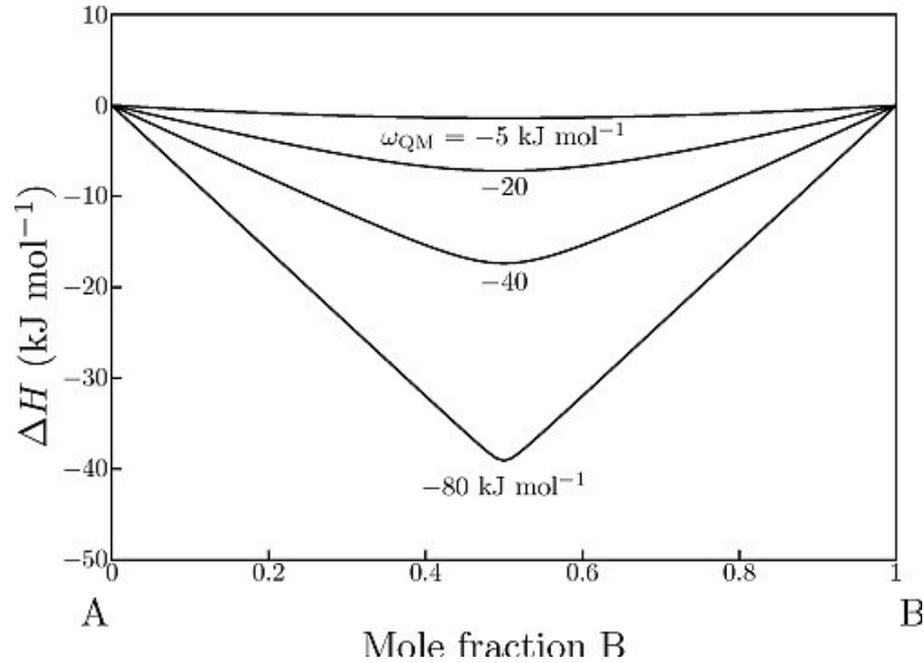


## Configurational entropy

$\omega_{AB} = 0 \rightarrow$  ideal entropy

$\omega_{AB} < 0 \rightarrow$  ordered solution  
(AB pair formation)

# Short range ordering : Quasi-chemical model



# Short range ordering : Quasi-chemical model

- Modification of Pelton & Blander (1984,1986)
  - The minimum of the mixing enthalpy (=maximum short ranager order) can be shifted  
→ equivalent fractions replace mole fractions of the species
  - Consequence: the Ising configurational entropy is no longer exact and becomes an approximation
  - Pair formation energy becomes composition dependent  
→ the enthalpy curve can be modelled more round
- Modification from Pelton&Chartrand
  - Introduction of two sublattices (cations/anions) to describe first neighbor / second neighbor interaction  
→ quadruplets

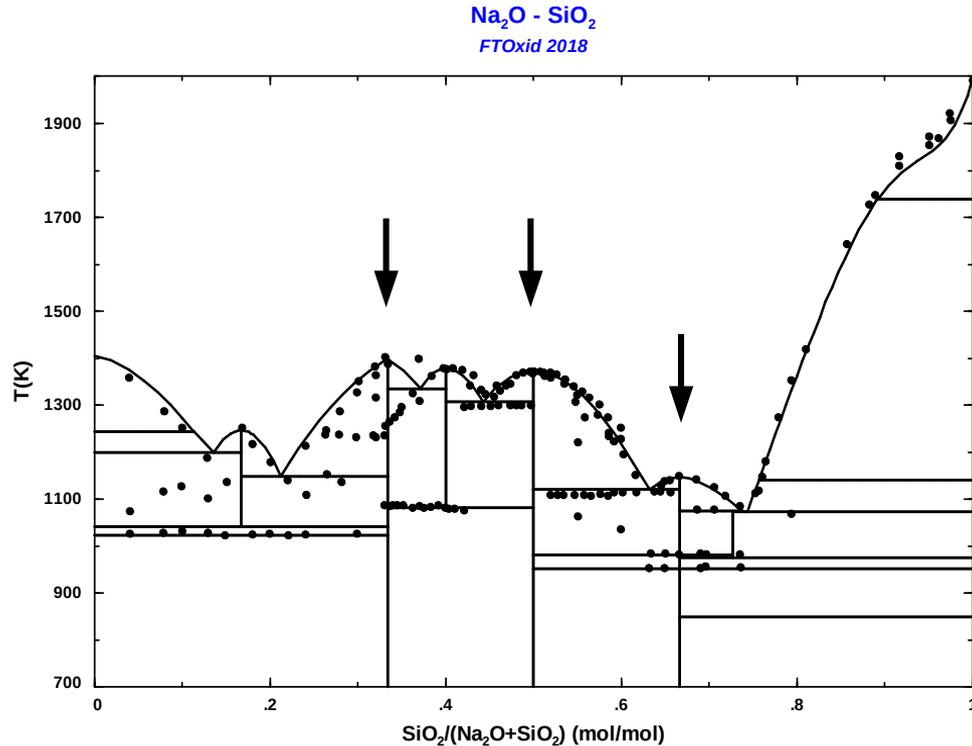
Example: Metal-Si-O-Cl

unary quadruplet: Si-O-Si-O ...

binary quadruplet: Si-O-M-O, Si-O-Si-Cl ...

reciprocal quadrulplet: Si-O-M-Cl

# Quasi-chemical model : $\text{Na}_2\text{O}-\text{SiO}_2$

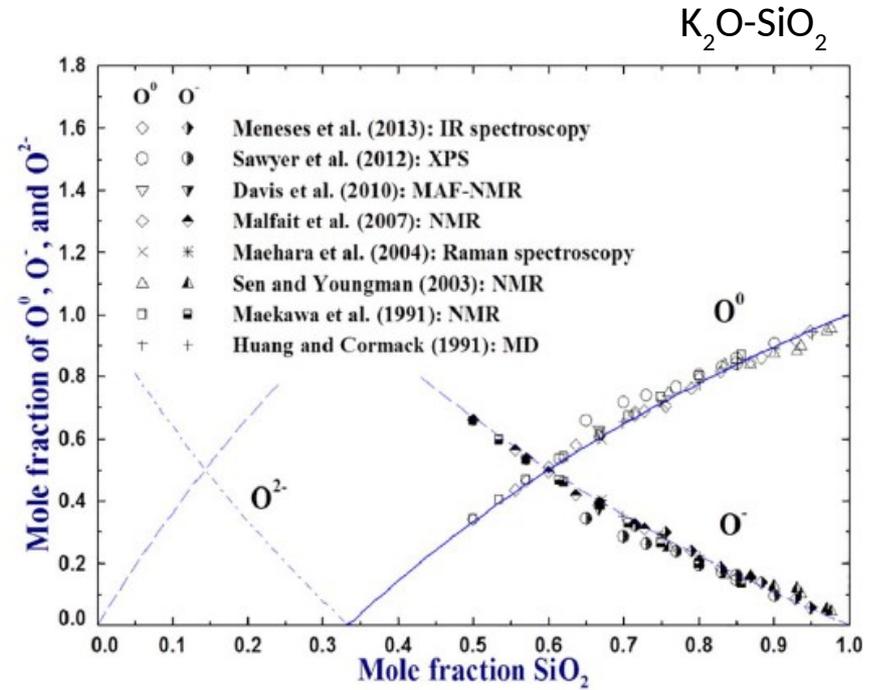
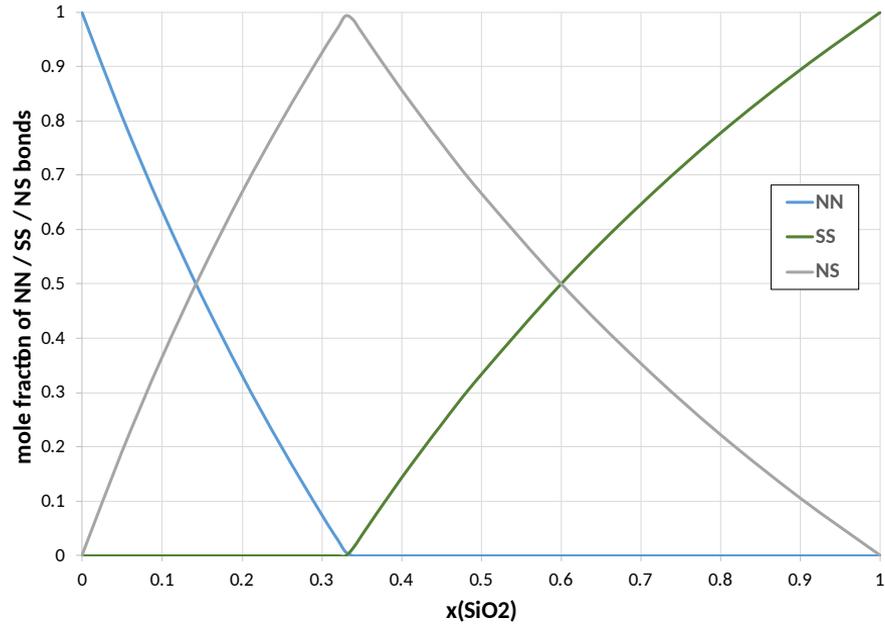


Experimental  
 $\text{Q}^4, \text{Q}^3, \text{Q}^2$

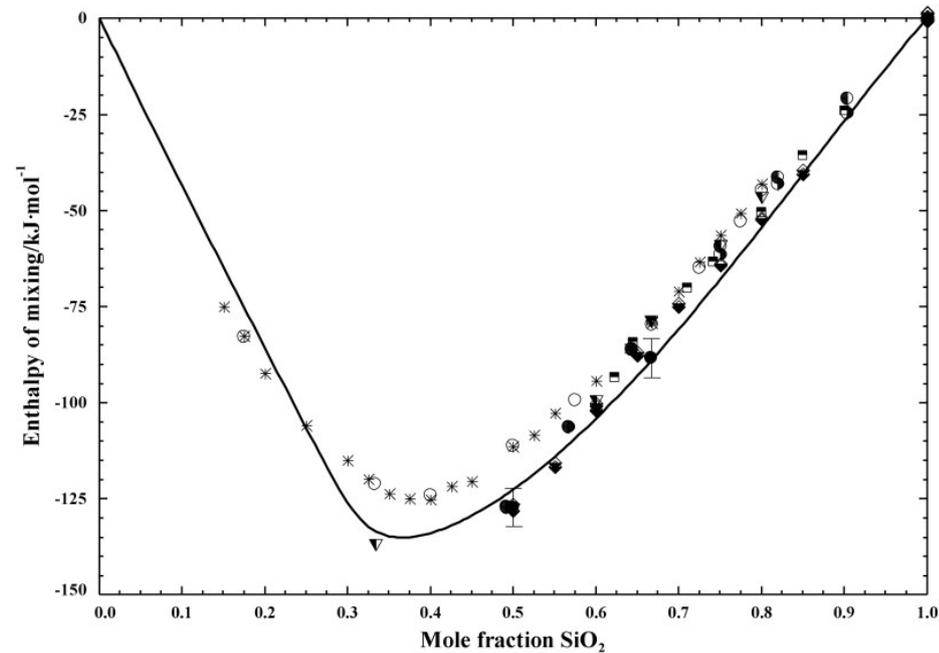
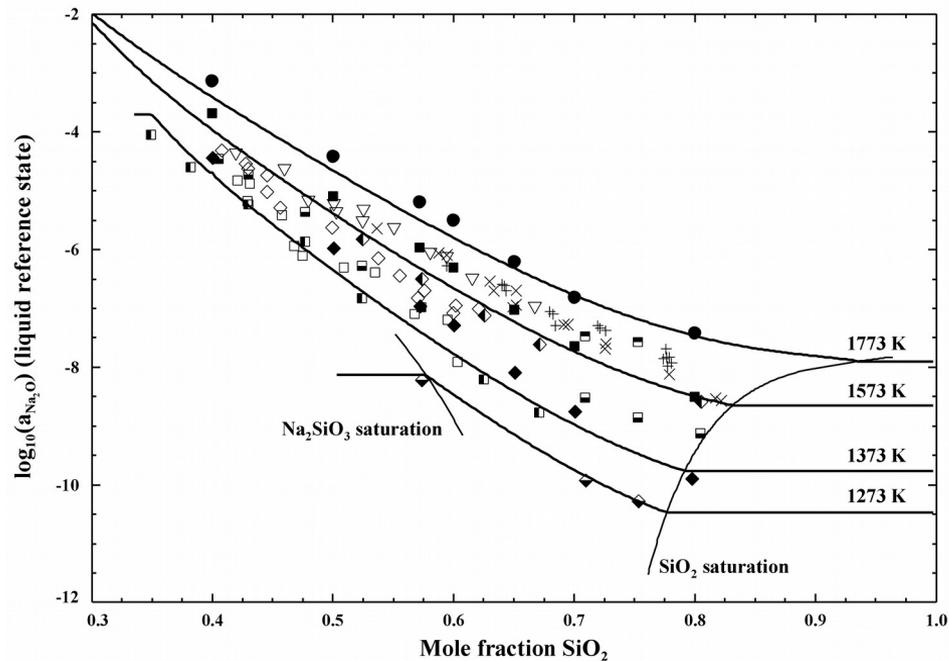
Associate model  
 $\text{SiO}_2, \text{Na}_2\text{Si}_2\text{O}_6, \text{Na}_2\text{SiO}_3, \text{Na}_4\text{SiO}_4, \text{Na}_2\text{O}$

Quasi-chemical model  
 $\text{Na-O-Na}, \text{Si-O-Si}, \text{Na-O-Si}$

# Quasi-chemical model : $\text{Na}_2\text{O}-\text{SiO}_2$



# Quasi-chemical model : $\text{Na}_2\text{O}-\text{SiO}_2$



# Quasi-chemical model : Q<sup>n</sup> species

- From pair fractions → Q species

total O in liquid:  $n_t = \frac{1}{2} x(\text{NaO}_{0.5}) + 2x(\text{SiO}_2)$

bridging O  $n_o$  for Si-Si pairs:  $n_o = x(\text{Si-Si}) * n_t$

amount of  $x(\text{SiO}_2)$  in 1 mol liquid :  $2 n_o / x(\text{SiO}_2)$

Probability that O is a bridging O

$$p = (2 n_o / x(\text{SiO}_2)) / 4 = n_o / 2x(\text{SiO}_2)$$

Equivalent fraction of SiO<sub>2</sub>

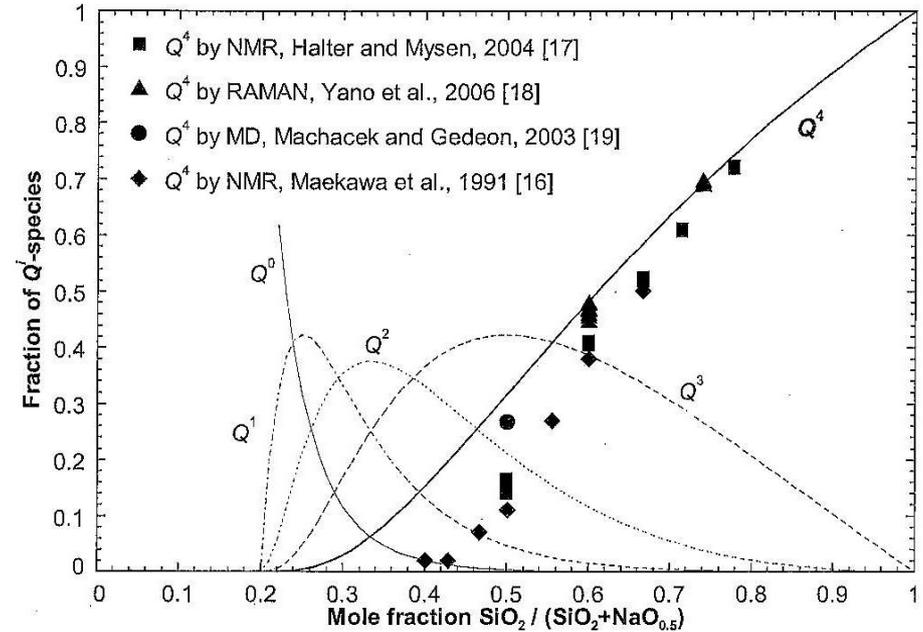
$$Y(\text{SiO}_2) = 4 x(\text{SiO}_2) / (4x(\text{SiO}_2) + x(\text{NaO}_{0.5}))$$

$$\rightarrow p = x(\text{Si-Si}) / Y(\text{SiO}_2)$$

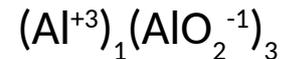
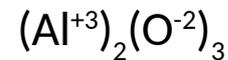
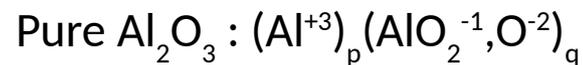
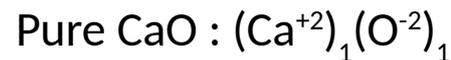
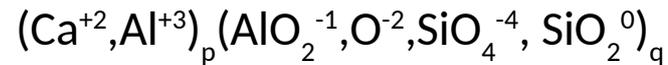
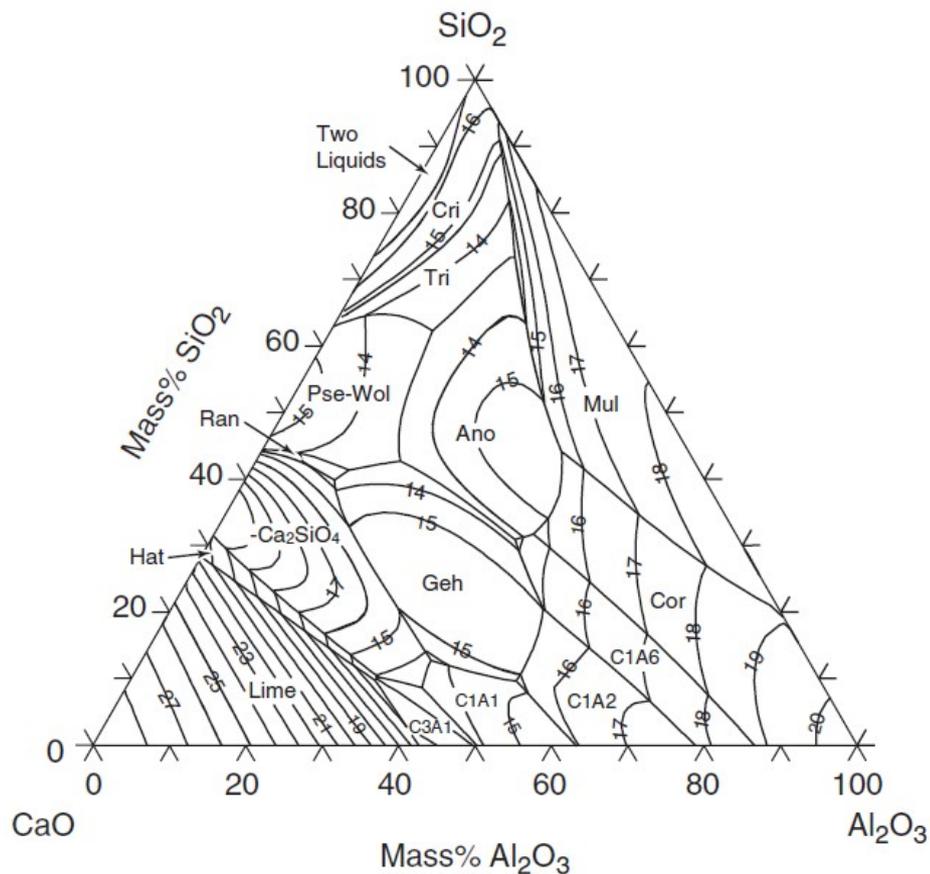
Use binomial distribution to calculate Q<sup>n</sup>

$$Y(Q^4) = p^4 ; Y(Q^3) = 4p^3(1-p) ; Y(Q^2) = 6p^2(1-p)^2$$

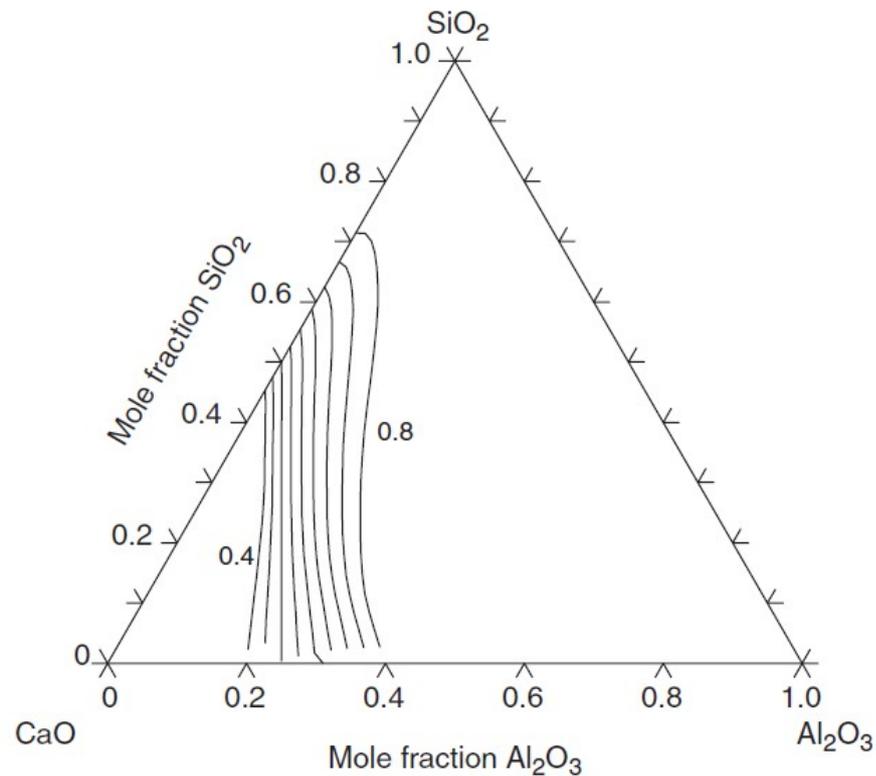
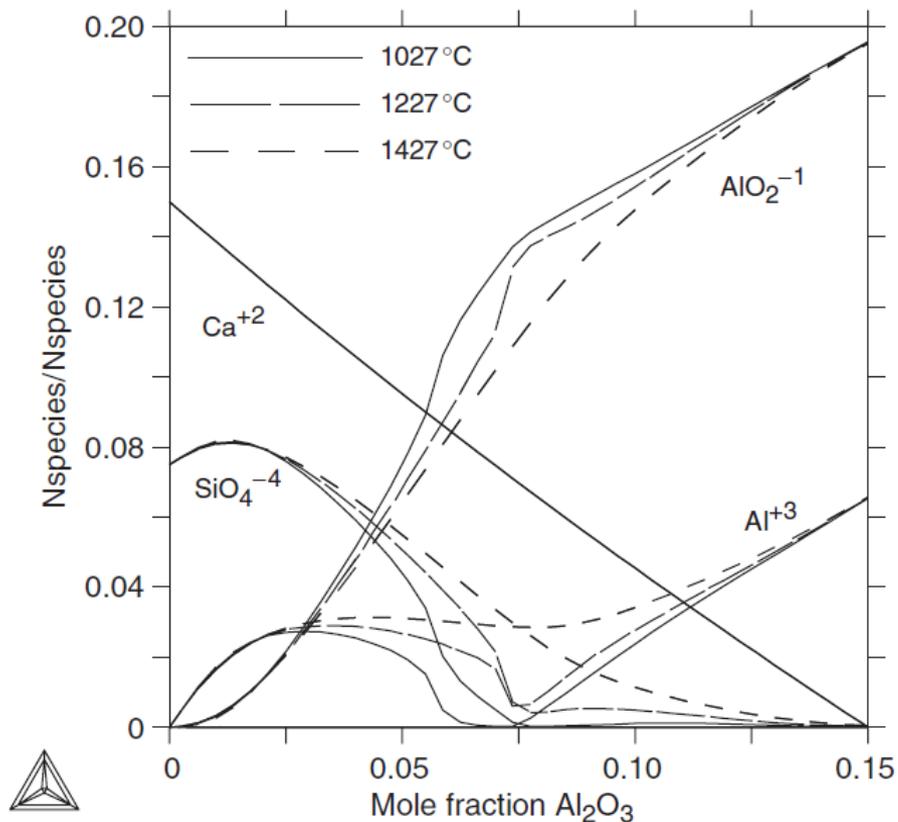
$$Y(Q^1) = 4p(1-p)^3 ; Y(Q^0) = (1-p)^4$$



# Ionic liquid model



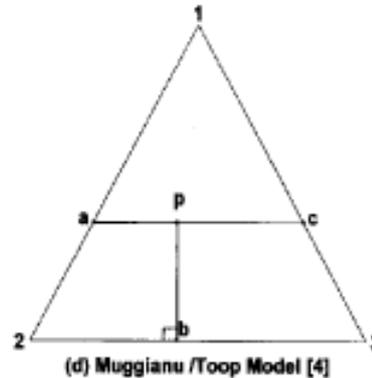
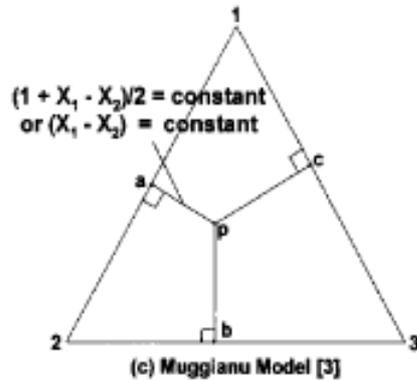
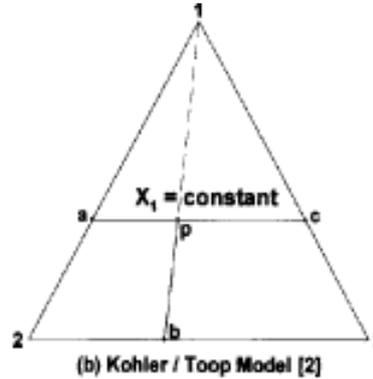
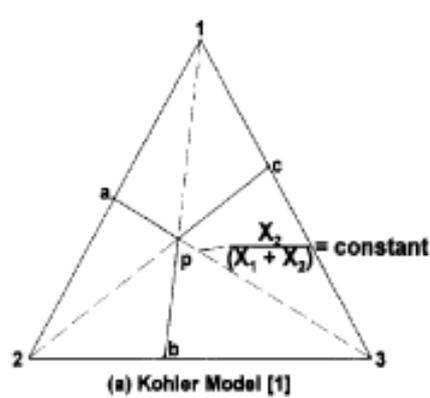
# Ionic liquid model



**Fig.14.** Calculated iso-concentration lines for the amount of  $y_{\text{SiO}_2^0} + y_{\text{AlO}_2^{-1}}$ , between 0.4 and 0.8, with a 0.05 interval at 1900°C.

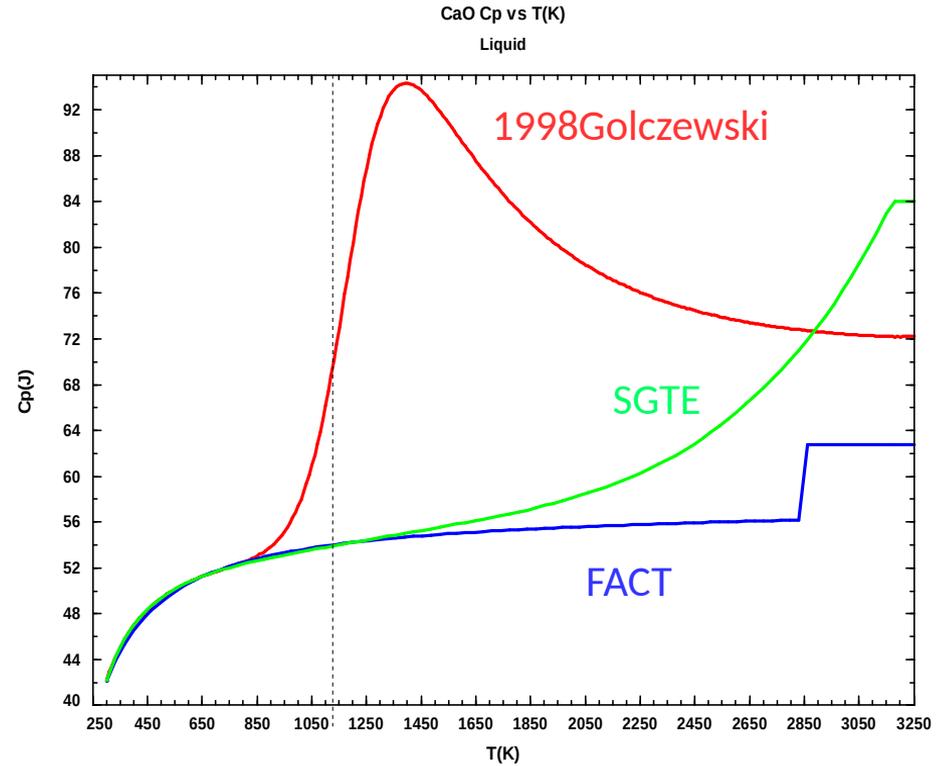
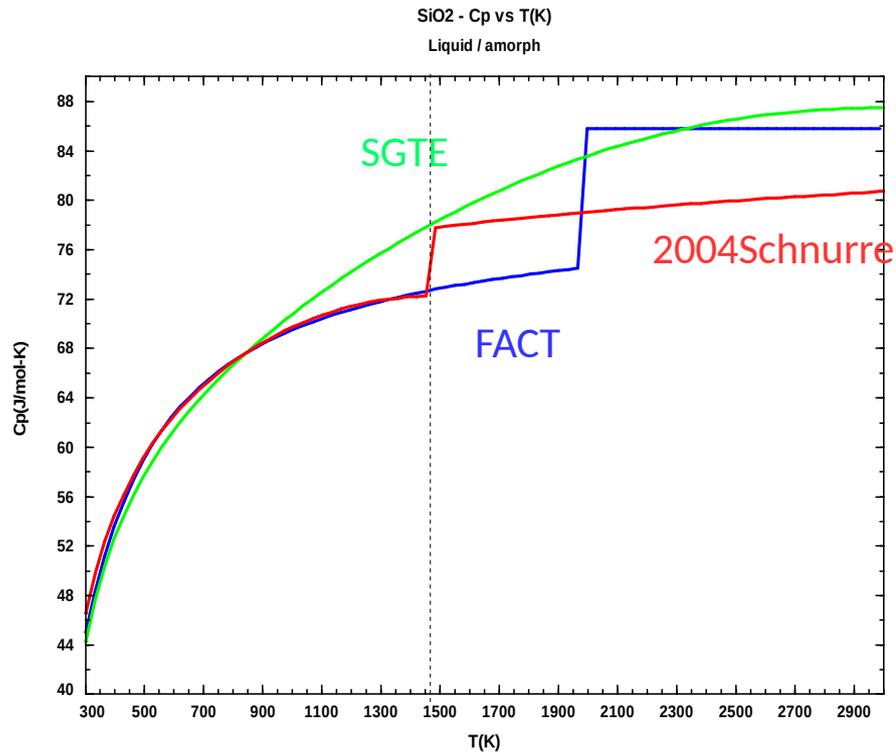


# Calphad modeling: Higher order extrapolation

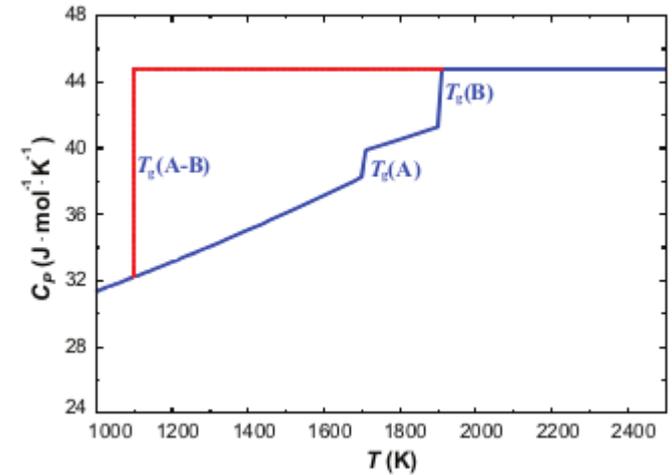
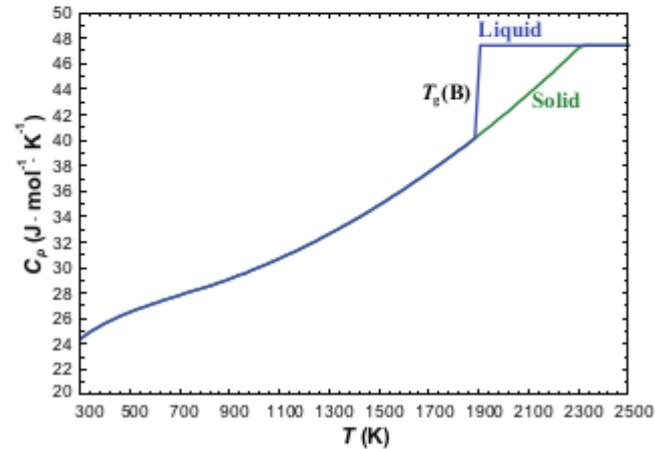
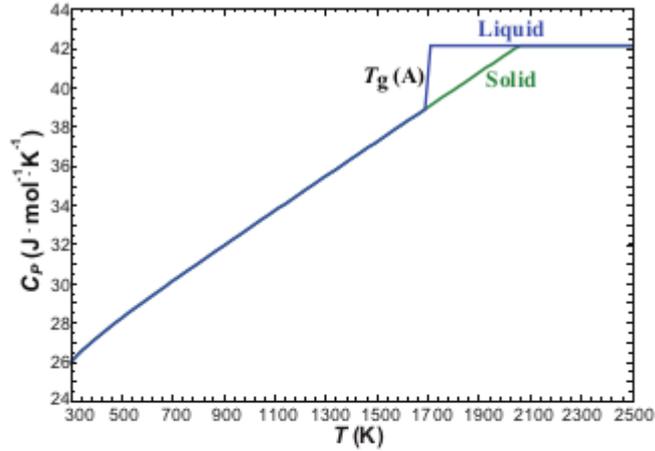


Extrapolation of binary systems into ternary and higher order systems

# What about the glass transition ?



# What about the glass transition ?



# Two-state model

Atoms are either “solid-like” or “liquid-like” and the Gibbs energy difference between the two is  $\Delta G_m^d$

$$\Delta G_m^d = G_m^{\text{liq}} - G_m^{\text{sol}} = H_m^{\text{liq}} - H_m^{\text{sol}} - RT + \dots,$$

The Gibbs energy for the liquid phase at any given temperature becomes

$$G_m^L = G_m^{\text{sol}} + \chi \Delta G_m^d + RT((1 - \chi) \ln(1 - \chi) + \chi \ln \chi).$$

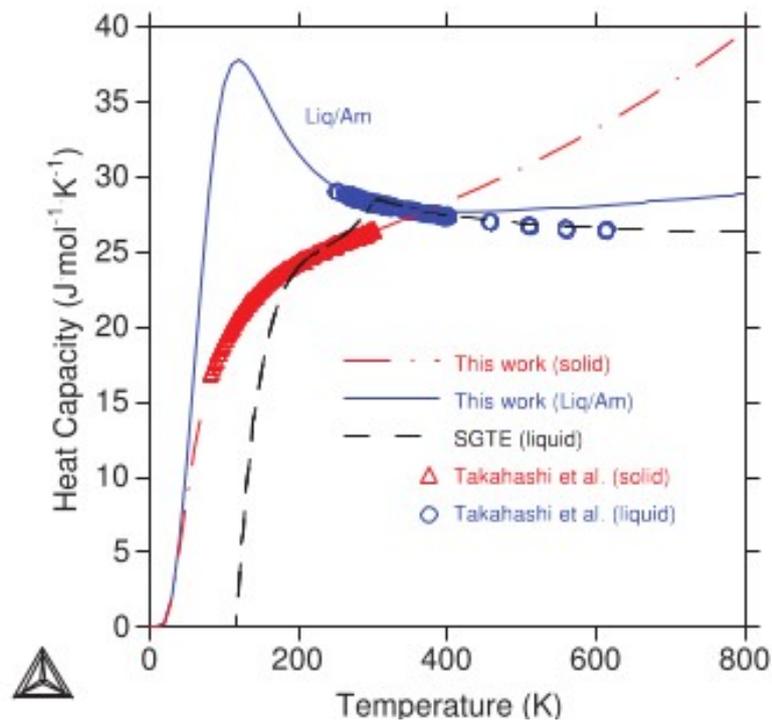
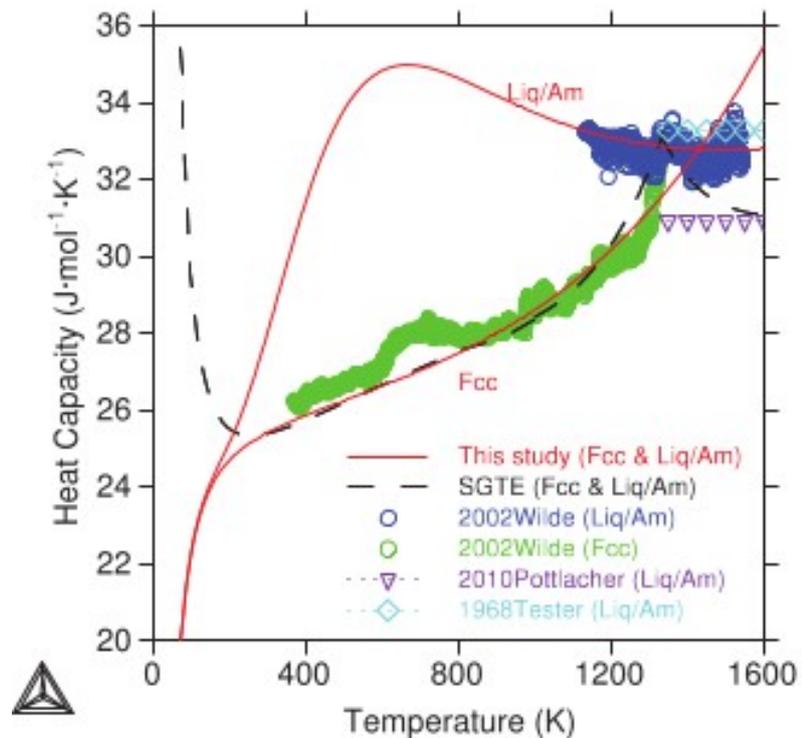
$\chi$  is an internal order parameter and can be solved analytically by calculating  $\partial G_m / \partial \chi = 0$

$$\chi = \frac{\exp(-\Delta G_m^d / RT)}{1 + \exp(-\Delta G_m^d / RT)}.$$

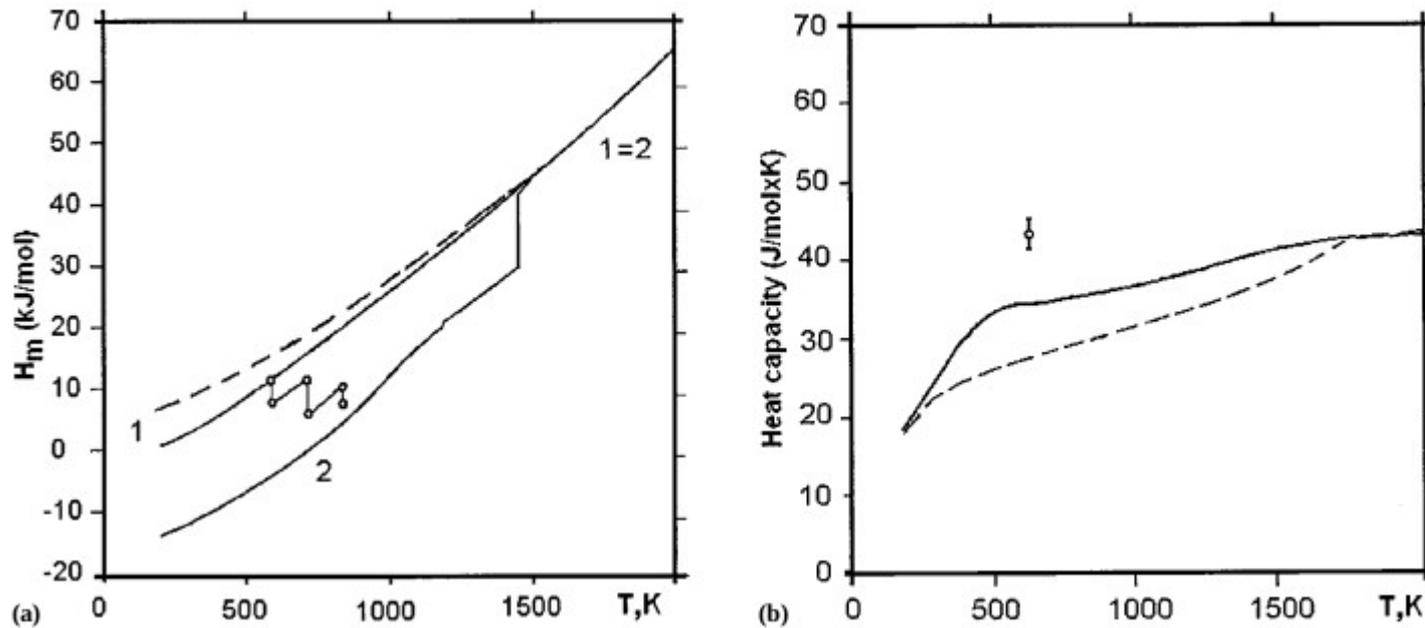
The Gibbs energy for the liquid phase becomes

$$G_m^L = G_m^{\text{sol}} - RT \ln \left( 1 + \exp \left( \frac{-\Delta G_m^d}{RT} \right) \right).$$

# Two-state model



# Two-state model



$Fe_{85}B_{15}$  amorphous sample : dotted line SGTE, solid Two-state

# Conclusions

- The Calphad method allows to model the thermodynamic properties of the liquid/amorphous phase
- Three different thermodynamic models are currently applied to model short range order
  - Associate model (Q-species)
  - Quasi-chemical model (bonding)
  - Ionic liquid model
- Structural features of the liquid are generally well reproduced
- Modeling of the glass transition is still a challenge
  - Two state model is promising, but only applied to elements / binary metallic systems
- Large databases are available commercially
  - >20 elements for metallic systems
  - >10 components for oxides systems