

Thermochemistry of magmatic degassing

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Andy Warhol, 1985

ICG Thermodynamic school – Erlangen May 2012, 2019 OUTLINE

- Introduction: the problem of volcanic degassing; measurements and sources
- « solubility » models (better if we talk about « saturation »)
- Mixing properties of silicate melts
- Polymeric modeling of the iron oxidation state and sulfur solubility and speciation



Introduction: volcanic and hydrothermal gases

Volcanic

	t °C	H2O	CO2	SO2	H2S	HCI	HF	H2	N2	CH4	CO
Erta Ale	1130	794000	104000	67800	6200	4200	tr	14900	1800	tr	4600
Klyuchevskoy	1100	977300	1200	900	20	14200	2500	5900	40	0.1	12
Mutnovsky	360	987000	5190	4020	1640	975	260	884	156	0.1	0.5
Mount Usu	690	993000	3600	320	180	340	60	2000	104	5.7	0.5
Ngauruhoe	640	960000	16050	10200	6800	2500	-	1420	1500	0.3	42
Papandayan	400	960000	29400	6750	2900	1250	33	140	550	0.6	0.3
Mt St Helens	540	985000	9130	730	1370	890		2440	470	0.2	13
Satsuma Iwo J,	880	973000	5100	8180	1640	5306	277	6070	80	4	17.2
Sierra Negra	280	311000	672000	12450	2700	275	21	3	1520	0.3	0.2
Showa Shinzan	800	980000	12000	430	4	530	240	6300	570	7.1	33
Tokachi	505	931000	11520	32570	21460	2760	345	120	224	0.1	1.1
Vulcano	620	861000	119000	6800	4800	4530	1010	1510	1068	0.1	110

Hydrothermal

	t °C	H2O	CO2	SO2	H2S	HCI	HF	H2	N2	CH4	CO
Solfatara-BG (2)	160	824529	173383	nd	1341	nd	nd	255.7	637	17.4	0.440
Vesuvio-FC1 (2)	99	982000	17750	nd	23	nd	nd	185	34.2	13.3	1.600
Pantelleria-F (2)	100	967900	23210	nd	tr	nd	nd	1220	6800	884.0	0.056
Vulcano-Vi (2)	99	936100	61200	nd	1478	nd	nd	654	509	66.0	0.056
Vulcano-Vsf (2)	98	906600	89970	nd	2309	nd	nd	108.7	867	115.8	0.100
Lipari-K1 (2)	96	852800	139700	nd	242	nd	nd	102	1820	5330.0	0.045
Ischia-DR (4)	99	997200	2655	nd	73	nd	nd	34.7	31.6	0.4	0.023
Tambora (5)	150	995500	3756	nd	389	nd	nd	268	46.2	4.5	0.045
Teide (6)	83	824300	174400	nd	171	nd	nd	492	660	3.9	0.290
Montserrat-L1 (9)	100	952000	43800	nd	3700	nd	nd	47	390	300.0	0.028
Kizildere (10)	94	638200	355000	nd	0	nd	nd	16.3	3740	2190.0	0.580
Larderello-Mr1 (2)	99	988700	10020	nd	352	nd	nd	380	119	434.0	0.011
Nisyros-1 (11)	98	985000	12460	nd	2340	nd	nd	120	54.1	72.7	0.067

Cold

	t °C	H2O	CO2	SO2	H2S	HCI	HF	H2	N2	CH4	CO
Mefite	13	nd	980000	nd	3580	nd	nd	80.7	14300	2130.0	0.480
Selvena	15	nd	885000	nd	12500	nd	nd	5140	17000	80400.0	9.500
Amiata	7	nd	960700	nd	1750	nd	nd	0.955	23580	13980.0	0.148
Umbertide	9	nd	923000	nd	nd	nd	nd	2	74400	2520.0	0.120
Caldara	11	nd	974000	nd	13100	nd	nd	5	12600	206.0	0.270



Techniques

- (i) DIRECT SAMPLING AND ANALYSIS IN LAB <u>allows</u> all major volcanogenic components (H₂O, CO₂, SO₂, HCl, ect.) to be simultaneously measured
 - <u>Main problem</u>: hazardous; time-consuming; Need to measure both: <u>intensive parameters: composition</u> = relative abundance of major species on air-free basis (direct sampling) <u>extensive parameters: fluxes = mass of a given species</u> emitted in unit time (e.g., tonnes per day)
- (ii) **REMOTE SENSING**; bulk (total) volcanic gas measurement from a distal location:

<u>Main problem</u>: the <u>atmosphere</u> contains high and variable H_2O and CO_2 contents. <u>Focus on SO_2</u>

(iii) MultiGAS

....and also

iv) Soil Gas measurements of hydrothermal areas



FTIR measurements of the emissions from the 2750 m. a.s.l. cone during the 2002 eruption of Mount Etna (Courtesy of Mike Burton, INGV Catania).

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-Large CO₂ fluxes contrast with relatively little volumes of erupted magma

-Full plume characterization

(b)

Lava lake

Spectrometer





 $log(fO_2) = A / T + B + C(P-1) / T$ (P en bars, T en Kelvins)



Tholeite

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Multi-GAS measurements

[Aiuppa et al, 2006, 2007, JGR, Geology]



• The Multi-GAS (Multi-component Gas Analyzer System), a custom-made instrument for detection of H₂O, CO₂, SO₂, H₂ and H₂S concentrations in volcanic plumes;

• developed in Italy (INGV-Pa) and Japan (H. Shinohara) in the early 2000's;

<u>In-situ method</u>: gas is pumped in the sensors and measured (no remote sensing; interference from atmosphere reduced)

Sensors: CO₂ (and H₂O): IR spectrometry H₂S, SO₂: electrochemical sensors

Automatic and semi-real-time 1 measure every 2-9 seconds

Telemetry

Automatic datalogging and radio transfer to Palermo



Fig.5. Horizontal and vertical concentration profiles of H2S in SC and TAS volcanic plumes in March 2012. Maps show (a) the summit lava dome and (b) the area of SC and TAS craters and their plumes. Variations in H₂S concentration along X (borizontal distance) and Y (height above ground) in the ellipsoidal cross section of both plumes are depicted by the colour scale from blue (low values) to dark red (high values). These were calculated from the horizontal and vertical profiles shown in (c, d) and (e), and by combining Eqs. (1) and (2) (see text). (c) Horizontal H₂S concentration profile across TAS volcanic plume (1.2 m height above the ground); (d) cumulative horizontal H₂S concentration profile, obtained by summing the results of all MultiGAS traverses orthogonal to the SC plume; and (e) vertical profile (Y, in m) of H₂S concentrations (Z, in ppm) obtained in the core of SC plume (e.g., at horizontal distance X = 43 m from A, along the track A–D of Fig. 4).

Contents lists available at ScienceDirect

Chemical Geology

journal homepage: www.elsevier.com/locate/chemgeo

Steam and gas emission rate from La Soufriere volcano, Guadeloupe (Lesser Antilles): Implications for the magmatic supply during degassing unrest

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CrossMark



Aiuppa et al. (2009)

CC Thormodynamic school – Erlangen Ma













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Soufrière de Guadeloupe (France) outlet at 100°C

Solfatara (Campi Flegrei, Italy outlet at 145-160°C

The thermo-fluid-dynamical modeling $(H_2O + CO_2 \text{ fluid})$ of hydrothermal systems



- Real gas at 15 Mpa and 350°C \rightarrow Single gas, h = 2220 J/g
- Ideal mixture → h = 2000 J/g, but at 15 MpaT is 320°C !!! → So it MUST be a two-phase (L+V) sysetm

Troise et al. (2019, ESR) Moretti et al. (submitted)

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Oppenheimer et al., 2011

Moretti et al., 2018

To draw, we look at magma...and its liquid phase: THE MELT

ICG Thermodynamic school – Erlangen May 2012, 2019 Measuring Initial Magmatic Volatiles What is the challenge in accurately measuring/estimating amount of volatiles

in magmas?

- When gas samples taken at surface, they can become contaminated with atmosphere or other secondary sources (meteoric waters etc...)
- If magma saturated and bubbles formed, lost some of its volatile supply prior to eruption

IWe can use "Phase Equilibria" or. May 2012, 2019

Glasses and Melt Inclusions



FIGURE 8 Glass (melt) inclusions in crystals from volcanic rocks. (A) A fragment of an \sim 3-mm quartz phenocryst from the rhyolitic Bishop Tuff containing inclusions of glass up to about 100 μ m in diameter. (B) Close-up of a melt inclusion containing

- Can measure abundances in submarine glasses because little to no degassing invoked; magma cools on contact with seawater
- Melt inclusions, which are blobs of melt (glass) surrounded by crystal.
- Interpretation is that these blobs of melt do not lose volatiles because "armored" by solid crystal.





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Then we need « solubility » models or to be more precise modeling of gas-melt interactions able to **precisely** calculate the saturation surface of the H₂O-CO₂-H₂S-SO₂ (+ Cl, F) – silicate melt system and see how magma degasses under varying P and T

Understanding solubilities and saturation properties²⁰¹⁹ demands first experiments...then "thermodynamics"



- Solubilities are strongly pressure dependent
- Solubilities do not vary much with composition
- CO₂ has very low solubility compared to H₂O (~30x lower)

How was the solubility of water assessed?²⁰¹⁹



For the reactive solubility of CO₂ in melts (Fine 19 and Stolper, 1989)

$$CO_{2(\text{fluid})} + O^{2-}_{(m)} = CO_3^{2-}_{(m)}$$
 (1)

Basalts: CO2 as carbonate ion only Rhyolites: CO2 as molecular CO2 only

Then, it is considered that: $K = X_{CO_3^{2-},m} / (f_{CO_2} X_{O^{2-},m})$ (2) $K = K^{\circ} \exp[(-\Delta V^{\circ}(P-P^{\circ})/RT) - (\Delta H^{\circ}/R) (1/T - 1/T^{\circ})]$ (3)

Surprisingly, $X_{O^{2-},m}$ is given as:

$$X_{O^{2-},m} = 1 - X_{CO_3^{2-},m}$$
 []] (4)

(but what about $2 O_{(m)}^{-} = O_{(m)}^{\circ} + O_{(m)}^{2-}$???)

Solubilities with more than 1 volatile component present 2019



- In natural systems, melts are saturated with a multicomponent vapor phase
- H₂O and CO₂ contribute the largest partial pressures, so people often focus on these when comparing pressure & volatile solubility

Let us consider ideal gas ($P_{TOT} = P_{H2O} + P_{CO2}$) and let us forget speciation phenomena in the melt phase (very simple



$$\mathsf{P}_{\mathsf{CO2}} = \mathsf{K}_{\mathsf{H},\mathsf{CO2}} \, \mathsf{C}_{\mathsf{CO2}}$$

with

$$P_{H2O} = 103.57 W_{H2O}^{1.9532}$$

Look at violet points and lines in the next slide !



The penguin is unhappy and wants more accurate equations for both liquid and gas phases !

CG Thermodynamic school – Erlangen May 2012, 2019
 S solubility is more complicated because of multiple oxidation states

- Dissolved S occurs as either S²⁻ or S⁶⁺
- Solubility is limited by sat'n with pyrrhotite, Fe-S melt, anhydrite, or CaSO₄ melt
- S in vapor phase occurs primarily as H_2S and SO_2



Figure 2. Solubility of sulfur in silicate melts at conditions of a fixed mole fraction of SO₂ in the input gas phase and varying fo, measured by Fincham and Richardson (1954) in a CaO-Al₂O₃-SiO₂ melt at 1 bar pressure. Please see text for further discussion of the reactions portrayed in these figures.

Baker and Moretti (2011)

Jugo (2005)

Oxidation state, ΔFMQ

So, we also need to describe RedOx properties

ICG Thermodynamic school – Erlangen May 2012, 2019 Depolymerization of Silicate Melts to accommodate volatiles (e.g. water)



Question: how much we need to know about structure ?

Answer: the amount of knowledge enough to describe speciation (e.g., same as in aqueous solution) and write reactions

Comment 1: this implies consistent choices for the thermodynamic state of reference Comment 2: it also implies the choice of a well performing model for melt mixing properties ICG Thermodynamic school – Erlangen May 2012, 2019 Silicate melts are not liquid water...

Outer sphere ion pair





Intact solvation shells



(complex)



Partial disruption of solvation shells

Disruption of solvation shells

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How deep need we to go with connections between structure and chemical thermodynamics ?

The "thermochemical knowledge" of a melt system does not seem to require the microstructural "complexity" that can be revealed by many spectroscopic investigations: the structural "characterization" exceeding that required for the description of acid-base properties (e.g, in the Lux-Flood notation for oxide systems) may be not useful.

ICG Thermodynamic school – Erlangen May 2012, 2019 Back to basics

In silicate melts acid-base properties are expressed in terms of Lux-Flood formalism:

Acid + $O^{2-} \Leftrightarrow Base$ (1)

(Ottonello et al., 2001; Moretti, 2005; Moretti and Ottonello; 2003; Ottonello, 1997: "Principles of Geochemistry"; Flood and Forland, 1947; Fraser, 1975; 1977).

In oxide systems, "reaction" 1 is the analogous of the Bronsted-Lowry one in aqueous solutions:

Acid \Leftrightarrow Base + H⁺ (2)

In aqueous solutions the electrode of reference is the "normal hydrogen electrode", whereas in silicate melts the reference electrode is the "normal oxygen electrode" (Ottonello et al., 2001), i.e.: $1/2O_2 + 2e^- \Leftrightarrow O^{2-}$ (3)

This is the main redox couple in oxide melts.

ICG Thermodynamic school – Erlangen May 2012, 2019 O²–? Virtual or real?

Journal of Non-Crystalline Solids 357 (2011) 170-180



Bridging, non-bridging and free (O²⁻) oxygen in Na₂O-SiO₂ glasses: An X-ray Photoelectron Spectroscopic (XPS) and Nuclear Magnetic Resonance (NMR) study H.W. Nesbitt ^{a,*}, G.M. Bancroft ^b, G.S. Henderson ^c, R. Ho ^a, K.N. Dalby ^a, Y. Huang ^b, Z. Yan ^b

As has been proposed for CaSiO₃ glass and for sodic and potassic glasses containing La, we suggest that O^{2-} is present in sodic glasses at small concentrations. The O^{2-} content correlates with increased soda content and may be associated with, and instrumental in development of, three dimensional percolation channels in the glasses

ICG Thermodynamic school – Erlangen May 2012, 2019 Polymeric nature of anion matrix: Toop-Samis model

In polymeric models for silicate melts, it is postulated that, <u>at each</u> composition, for given P-T values, the melt is characterized by an equilibrium distribution of several ionic species of oxygen, metal cations and ionic polymers of monomeric units SiO_4^{4-} .



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Theory: the polymeric model

On the basis of simple mass balances we can link the three oxygen species to the melt composition and therefore to the melt compositions

$$(O^{0}) = \frac{4N_{SiO_{2}} - (O^{-})}{2} (O^{2-}) = (1 - N_{SiO_{2}}) - \frac{(O^{-})}{2} (O^{-})^{2} (4K_{2} - 1) + (O^{-})(2 + 2N_{SiO_{2}}) + 8N_{SiO_{2}} (N_{SiO_{2}} - 1) = 0$$

 $Kp = (O^{\circ})(O^{2})/(O^{-})^{2}$

ICG Thermodynam CaO-SiO₂ – Erlangen May 2012, 2019



Ottonello (2001) Ottonello and Moretti (2004)

Join MOUY	$\ln Kp = A/$	T+B	\mathbb{R}^2	T range	Notes 2
	А	В	С	(°C)	
$\overline{K_2O - SiO_2}$	-31708	0	_	1127-1527	(1)
	-29540	0	-	1223	(2)
	-36967	0	0.9922	1500-1800	(3)
Na_2O-SiO_2	-23336	0	0.9995	1000-1800	(3)
CaO - SiO_2	-15372	0	0.9958	1000-2000	(4)
	-14807	0	0.9943	1000-2000	(2)
MgO - SiO_2	-9809.5	0	0.9955	1400-2000	(3)
$ZnO - SiO_2$	-6460.1	0	-	1400-2000	(3)
$MnO - SiO_2$	-6183.8	0	0.9596	1000-2000	(3)
	-5649.1	0	-	1600	(1)
PbO - SiO_2	-5330.0	0	0.5825	1000-1800	(3)
	-4098.1	0	-	1273	(5)
FeO - SiO ₂	-3600.0	0	0.9973	1000-2000	(4)
$Fe_2O_3 - SiO_2$	7569.5	- 7.2752	0.9350	1000-2000	(5)
TiO_2 - SiO_2	4667.3	-3.2092	0.9107	1500-1900	(3)
$ZrO_2 - SiO_2$	2685.9	- 6.382	0.9658	1400-2000	(3)
$NiO - SiO_2$	1507.7	- 1.7772	0.9825	1500-2000	(3)
Al_2O_3 - SiO_2O		- 1.4059	-	1000 - 2000	(3)
B_2O_3 - SiO_2O		- 1.0660	-	1000 - 2000	(3)

(1) Ottonello (2003); (2) Ottonello and Moretti (2003), based on experiments of Eliezer et al. (1978);
(3) Ottonello and Moretti (2003), based on the Modified Quasi Chemical parameterization of Pelton et al. (1995); (4) Ottonello (2001); (5) Ottonello et al. (2001)

Ottonello and Moretti (2004)

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Ottonello et al., 2001

ICG Thermodynamic school – Erlangen May 2012, 2019 Toop-Samis model embodies ideal and excess Gibbs free energy contributions to the Gibbs free energy of the liquid MO-SiO₂ mixture in a single term (0^{-1})

$$\Delta G_{\text{mixing}} = -\frac{(O^{-})}{2} RT \ln K$$

→ the amount of Gibbs free energy necessary to open a liquid solvus at high SiO₂ content can be seen as an elastic energy contribution which, for a chain of \overline{v}_{si} monomers extending to a distance x may be expressed (e.g. Bates and Fredrickson, 1999)

$$G_{\text{strain}} = \frac{3RT}{2\overline{v}_{\text{Si}}} \left(\frac{x}{a}\right)^2.$$
$$\frac{x}{a} = \chi_1 \cdot N_{\text{Sio}_2} + \chi_2 \cdot N_{\text{Sio}_2}^2 + \chi_3 \cdot N_{\text{Sio}_2}^3 + \chi_4 \cdot N_{\text{Sio}_2}^4 + \dots$$

Extended as: $\ln K_P = N'_{A^{v+}} + \ln K_{P,A-F} + N'_{B^{o+}} + \ln K_{P,B-F} + \dots$ $N'_{A^{v+}} = \frac{v_A^+ n_A}{v_A^+ n_A + v_B^+ n_B + \dots}$

ICG Thermodyn A « crude » approximation... May 2012, 2019



Ottonello et al., Chem. Geol. (2001)

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Even simple interaction parameters along limiting binaries cannot be reduced to fitting coefficients of mathematical minimization routines, but must be formally linked to the intrinsic atomistic properties of the interacting ions and molecules

In a chemically complex melt or glass the ability to transfer fractional electronic charges from the ligands to the central cation depends in a complex fashion on the melt or glass structure, which affects the polarization state of the ligand itself. Nevertheless, the mean polarization state of the various ligands (mainly oxide ions O^- and O^{2-} in natural silicate melts) and their ability to transfer fractional electronic charges to the central cation are conveniently represented by the "*optical basicity*" of the medium, i.e. ratio h/h^{*}, where h is Jørgensen's (1962) function of the ligand in the polarization state of interest, and h^{*} is the same function relative to the ligand in an unpolarized state (mainly free O^{2-} ions in an oxidic medium; Duffy and Ingram, 1971):

$$\Lambda = \frac{h}{h^*} = \frac{1 - \beta}{1 - \beta^*} = \frac{v_{\text{free}} - v_{\text{glass}}}{v_{\text{free}} - v^*}$$

with $v_{\text{free}} = {}^{1}S_{0} \rightarrow {}^{3}P_{1}$ absorption band of the free p-block cation; $v_{\text{glass}} = {}^{1}S_{0} \rightarrow {}^{3}P_{1}$ absorption band measured in the glass; $v^{*} = {}^{1}S_{0} \rightarrow {}^{3}P_{1}$ absorption band in a free O²⁻ medium. **ICG Thermodynamic school – Erlangen May 2012. 2019** The reciprocal of optical basicity Λ of a cation (i.e. "*basicity moderating parameter*" γ of Duffy and Ingram, 1973) represents the tendency of an oxide forming metal M to reduce the localized donor properties of oxide ions, and is related to the optical basicity of the medium by:

$$\gamma_{\rm M} = \frac{Z_{\rm M} \times r_{\rm M}}{\left| Z_{\rm o} \right| \times \Lambda_{\rm MO}}$$

where Z_M = formal oxidation number of cation in MO

- Z_0 = formal oxidation number of oxide ion in MO
- r_M = stoichiometric ratio between number of cations and number of total oxide ions in the medium.

Table I. Optical basicity Λ and basicity moderating parameter of the central cation γ according to various sources. Pauling's and Sanderson's electronegativities (Pauling, 1932, 1960; Sanderson, 1967) are also listed. Λ , γ , χs : adimensional; χ_P : eV (from Ottonello *et al.*, 2001).

2019

Oxide	Λ)	/	χр	χ_S	
	(1)	(2)	(3)	(4)	(5)	(6)	(6)	(7)			
$H_{2}O$			0.40)		0.39	2.56	2.50	2.15	3.55	
Li_2O						1.00	1.00		1.0	0.74	
B_2O_3			0.42			0.42	2.38		2.0	2.84	
Na ₂ O		1.15	1.15	1.15	1.15	1.15	0.87	0.87	0.9	0.70	
MgO	0.78	0.78	0.78	0.78	0.78	0.78	1.28	1.28	1.2	1.99	
Al ₂ O ₃	0.60	0.60	0.60	0.61	0.59	0.59	1.69	1.67	1.5	2.25	
SiO_2	0.48	0.46	0.48	0.48	0.48	0.48	2.09	2.09	1.8	2.62	

depolymerizing role of water has been overrated with respect to its actual acid-based properties in melts.

TiO_2		0.65		0.61	0.61	0.58	1.72	1.54	1.6	1.60
Cr_2O_3	0.70					0.58	1.72		1.6	1.88
MnO	0.94-1.03	0.98		0.90	0.59	0.59	1.69	1.69	1.5	2.07
FeO	0.86 - 1.08	1.03	1.00	1.03	0.51	0.48	2.09	1.354	1.8	2.10
Fe_2O_3	0.73-0.81	0.77		1.21	0.48	0.48	2.09	2.09	1.8	2.10
CoO						0.51	1.96	1.96	1.7	2.10
NiO						0.48	2.09	2.09	1.8	2.10
Cu ₂ O						0.43	2.30	2.30	1.9	2.60
ZnO	0	.82-0.98	8			0.58	1.72	1.72	1.6	2.84
SrO	1.10					1.03	0.97		1.0	1.00
SnO						0.48	2.09	2.09	1.8	3.10
BaO	1.15	1.15		1.15	1.15	1.12	0.89		0.9	0.78
РЬО						0.48	2.09	2.09	1.8	3.08

Duffy (1992); (2) Young et al. (1992); (3) Duffy and Ingram (1974a,b); (4) Sosinsky and Sommerville (1986); (5) Gaskell (1982); (6) Ottonello et al. (2001); eq. (4.19) (note that Λ=γ⁻¹); (7) Ottonello et al. (2001); obtained by non linear minimization of FeO thermodynamic activity data in multicomponent melts.

ICG Therm The H_2O - CO_2 - H_2S - SO_2 saturation model 012, 2019

Gas phase

$\mathrm{H_2O},\,\mathrm{CO_2},\,\mathrm{SO_2},\,\mathrm{H_2S}$

homogeneous equilibrium (chemical reactions)

(SUPERFLUID – Belonoshko et al., 1992)



ICG The Theory of the revised and extended H₂O-CO₂, 2019 saturation model (Papale, Moretti & Barbato, 2006)

- •Fully non-ideal
- •Fluid phase of any composition in the system H_2O+CO_2
- •Liquid phase of any composition from two/three components to natural (12 components)

Equilibrium equations

$$P^{G} = P^{L} = P$$
$$T^{G} = T^{L} = T$$
$$f^{G}_{H_{2O}} = f^{L}_{H_{2O}} \Longrightarrow \phi_{H_{2O}} y_{H_{2O}} P = \gamma_{H_{2O}} x_{H_{2O}} f^{oL}_{H_{2O}}$$

$$f_{CO_2}^G = f_{CO_2}^L \Longrightarrow \phi_{CO_2} y_{CO_2} P = \gamma_{CO_2} x_{CO_2} f_{CO_2}^{oL}$$

Mass balance
equations
$$y_{H_2O} + y_{CO_2} = 1$$
$$\frac{x_{H_2O}^T - x_{H_2O}}{y_{H_2O} - x_{H_2O}} = \frac{x_{CO_2}^T - x_{CO_2}}{y_{CO_2} - x_{CO_2}}$$







Barsanti et al. (2009, JGR)

)ol – Erlangen May 2012, 2019



...shifting degassing paths...

Heterogeneous large total CO₂ abundance in the shallow magmatic system of Kilauea volcano, Hawaii

Michele Barsanti, 1,2 Paolo Papale, 1 David Barbato, 1,3 Roberto Moretti, 4 Enzo Boschi, 1,4 Erik Hauri, 5 and Antonella Longo 1

ICG Thermodynamic school – Erlangen May 2012, 2019 $Fe^{2+} + 1/4 O_2 \Leftrightarrow Fe^{3+} + 1/2 O^{2-}$,

$$K_{3/2} = (a_{\text{Fe}^{3+}}/a_{\text{Fe}^{2+}}) (a_{\text{O}^{2-}})^{1/2} / f_{\text{O}_2}^{1/4},$$

 $\log (\text{Fe}^{3+}/\text{Fe}^{2+}) = \log K_{3/2} + 1/4 \log f_{O_2} - 1/2 \log a_{O^{2-}} = A - 1/2 \log a_{O^{2-}}$

Figure 10.12. Iron redox ratio of alkali silicate melts at 1400°C in air against SiO_2 concentration [Paul and Douglas, 1965]. Total iron content of 0.41 wt %.



variations of a_{O^2} with composition!???!

Figure 10.16 - Iron redox ratio against K/(K+Al) for potassium aluminosilicates at constant 78 mol % SiO₂ [Dickenson and Hess, 1981]. Experiments made in air at 1400°C with a total of 2 wt % FeO.



Empirical efforts....

$$\ln (x_{\text{Fe}_2\text{O}_3}/x_{\text{FeO}}) = a \ln f_{\text{O}_2} + b/T + c + \sum d_i x_i$$

$$\ln (x_{\text{Fe}_2\text{O}_3}/x_{\text{FeO}}) = a \ln f_{\text{O}_2} + b/T + c + \sum d_i x_i$$

$$+ e \left[1 - T_0/T - \ln T/T_0\right] + f P/T + g (T - T_0)P/T + hP^2/T_1$$

 $\ln (x_{\text{Fe}^{3+}}/x_{\text{Fe}^{2+}}) = a \ln f_{\text{O}_2} + b/T + c + d(\text{Al}/(\text{Al}+\text{Si}) + e(\text{Fe}^{3+}/\text{Fe}^{3+}+\text{Si}) + \sum f_i x_i$

Back to basics: amphoteric behavior of trivalent iron 2019

 $FeO + 1/4O_2 \Leftrightarrow FeO_{1.5}$

In the above reaction the redox potential is expressed by the oxygen fugacity. But how does the electron transfer take place?

$$Fe_{melt}^{3+} + e^{-} \Leftrightarrow Fe_{melt}^{2+} + Fe_{melt}^{2+} + Fe_{melt}^{2+} + e^{-} \Leftrightarrow Fe_{melt}^{2+} + 2O_{melt}^{2-} + \frac{1}{2}O_{2,melt}^{2-} \Leftrightarrow \frac{1}{4}O_{2,melt} + e^{-} = \frac{1}{2}O_{2,melt}^{-} \Leftrightarrow e^{-} + \frac{1}{4}O_{2,melt} = \frac{1}{2}O_{2,melt}^{-} \Leftrightarrow Fe_{melt}^{2+} + \frac{1}{4}O_{2,melt} = \frac{1}{2}O_{2,melt}^{-}$$

That's the way electron transfer operates. It is not evident from the equilibrium involving macroscopic components: to get that you must adopt the ionic notation.

ICG Thermodyna Iron sedox model langen May 2012, 2019

The message:

- 1. Silicate melts are polymerized liquids
- 2. Polymeric units are highly reactive

Polymerization and redox state are intimately interrelated. This melt affects properties, including oxidation state, volatile solubility *et cetera*.

$$\left(\frac{\text{Fe}^{II}}{\text{Fe}^{III}}\right) = \frac{n_{\text{Fe}^{II}}}{n_{\text{Fe}^{III}}} = \frac{[\text{Fe}^{2^+}]\sum \text{cations}}{[\text{Fe}O_2^-]\sum \text{anions} + [\text{Fe}^{3^+}]\sum \text{cations}}$$

$$\left(\frac{Fe^{II}}{Fe^{III}}\right) = \frac{1}{K_1 f_{O_2}^{1/4}} \times \frac{a_{O^{2-}}^{1/2} K_4 \sum cations}{K_2^{1/2} a_{O^{2-}}^2 \sum anions + K_3^{1/2} \sum cations}$$

Ratio of activitiesRatio of activity coefficients $(a_{FeO}/a_{FeO1.5})$ $(\gamma_{FeO1.5}/\gamma_{FeO})$

ICS solubility: the Conjugated-Toop-Samis (CTSFG) model 2019



Geochimica et Cosmochimica Acta, Vol. 69, No. 4, pp. 801–823, 2005 Copyright © 2005 Elsevier Lid Printed in the USA. All rights reserved 0016-7037/05 \$30.00 + .00

doi:10.1016/j.gca.2004.09.006



Moretti and Ottonello (2005 GCA)

Sulfide equilibrium:

$$O^{2-}(L) + \frac{1}{2}S_2(G) \Leftrightarrow \frac{1}{2}O_2(G) + S^{2-}(L)$$
Sulfate equilibrium:

$$O^{2-}(L) + \frac{1}{2}S_2(G) + \frac{3}{2}O_2(G) \Leftrightarrow SO_4^{2-}(L)$$



ICG Thermody Theory of the S solubility model (CTSFG) 2019

$$C_{S^{2-}} = \left[S\right]_{wt\%} \left(\frac{f_{O_2}}{f_{S_2}}\right)^{\frac{1}{2}}$$
$$C_{SO_4^{2-}} = \left[S\right]_{wt\%} f_{O_2}^{-\frac{3}{2}} f_{S_2}^{-\frac{1}{2}}$$

The model computes $C^{anneal.}$ (entropies of annealing). $k_{MO-(S2-,SO42-)}$ constants are from independent thermodynamic compilations when available. <u>Gas-liquid reactions:</u> Flood and Grjotheim (1952) thermochemical cycle:

$$\ln k_{S^{2^{-}},SO_{4}^{2^{-}}} = \sum_{i=1}^{N_{OX}} N_{i}^{v_{+}} \ln C^{anneal} k_{MO^{-}(S^{2^{-}},SO_{4}^{2^{-}}),i}$$
$$N_{i}^{v_{+}} = \frac{v_{i}^{*}n_{i}}{\sum_{i=1}^{N_{OX}} v_{i}^{*}n_{i}}$$

where $N_i^{\nu+}$ represent *electrically equivalent fractions*, and n_i are mole fractions computed over the appropriate matrix, either **cationic** or **anionic** (**Temkin model** of fused salts)

i=1

Fincham and Richardson (1954):

$$2O^{-} \Leftrightarrow O^{0} + O^{2-}$$

And Toop-Samis approach

ICG TIS solubility at P: considering volumes for systems 19 in which they have never been determined !

$$\ln K_{O-S,M}^{\prime P-T} = \frac{A_{O-S,M}^{\prime} + B_{O-S,M}^{\prime}}{T - \frac{1}{RT} \int_{1}^{P} \left(\Delta V_{m} + \Delta V_{g} \right) dP}$$

1-bar lnK

$$V_{M_{2/v^{+}}SO_{4}} = V_{M_{2/v^{+}}O} + V_{SO_{3}}$$

*Our value for the (partial) molar volume of V*₅₀₃ *is 57.71 cm³/mol at 1673K... <u>must be</u>* <u>checked experimentally (no data at present)</u>

$$\Delta V_{SO_4-S_2} = V_{M_{2/v^+}SO_4} - V_{M_{2/v^+}S} = 41 \text{ (cm}^3/\text{mol)}$$



Moretti and Ottonello (2003), Metall. Mat. Trans. B

Moretti and Ottonello (2005)

The CTSFG solubility model: features of the sulfide and 2019 sulfate capacity surfaces



Figure III.10: In C₈₀₄ calculated as explained in the text, versus total pressure.

Modeling the Solubility of Sulfur in Magmas: A 50-Year Old Geochemical Challenge



Figure 13. Comparison of the calculated molar ratio of S⁶⁺/Total S (X-S⁶⁺/Total S) in melts as a function of Δ NNO for basaltic and rhyolitic melts at different temperatures, pressures and water concentrations in the melt. Drawn after Moretti and Baker (2008). Note how unlike in Figure 8, the curves are functions of the intensive thermodynamic variables describing the melt, e.g., pressure, temperature and composition. Please see the text for further discussion.

Baker and Moretti (2011)





Moretti et al. (2003) Geol. Soc. Spec. Publ. 213

Mass partitioning in Nature is non-linear. The expected linearity required by theory (stoichiometry in this case) is embodied, not cancelled. Models must account for it.

A Model for the Saturation of C–O–H–S Fluids in Silicate Melts

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From: OPPENHEIMER, C., PYLE, D.M. & BARCLAY, J. (eds) *Volcanic Degassing*. Geological Society, London, Special Publications, **213**, 81–101. 0305–8719/03/\$15.00 © The Geological Society of London 2003.



ICG Thermodynamic school – Erlangen May 2012, 2019 Fe-S mutual interactions

We can also study the mutual redox exchanges between more redox couples (when existing...) such as Fe, Ni, S and so on... But even when studying mutual interactions, O²⁻ and therefore oxygen species via Toop-Samis equilibrium, intervene through the normal oxygen electrode (see Moretti and Ottonello, 2003 JNCS). For example, if you consider Fe and S redox equilibria you should write the following ionic equilibria:

 $8Fe_{melt}^{3+} + S_{melt}^{2-} + 4O_{melt}^{2-} \Leftrightarrow 8Fe_{melt}^{2+} + SO_{4,melt}^{2-}$

 $SO_{4,melt}^{2-} + 8Fe_{melt}^{2+} + 12O_{melt}^{2-} \Leftrightarrow S_{melt}^{2-} + 8FeO_{2,melt}^{-}$ If you write:

 $SO_{4,melt}^{2-} + 8FeO \Leftrightarrow S_{melt}^{2-} + 4Fe_2O_{3,melt}$

so that O²⁻ cancel out, you make a very huge mistake, since you are mixing different notations, confusing species with components and therefore mixing up standard states! <u>Remind that the basis of redox reactions in melts is the "normal</u>

oxygen electrode"

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volatiles in magmatic systems

ICG Ther some observations and caveats... 2019

We usually do not perceive the problem of the chemical syntax as long as we interpret our own data and a **few** more

➔ Thus we tend to adopt the detected structural scenario and turn it into the chemical syntax

- → we do not provide a thermodynamically coherent frame for acid-base e redox properties solving for speciation issues in melts/glasses and describing the ongoing chemistry
- → in general, too many structural attributions to the same REACTIVE species (Fe^{III}O₂⁻, Fe^{III}O₄⁻, Fe^{III}O₅⁻...) or no attribution at all (undifferentiated Fe³⁺ for all three-valent iron complexes)
- → inconsistent notations in the same reaction mechanisms → different standard states mixed-up